

OIL PALMIR JSC



**Crude Oil Refinery - Porto Romana - Durrës,
Albania**

BUSINESS PLAN

MARCH 2025

Preface

This business plan presents an opportunity for major investors to finance and manage the construction of a state-of-the-art oil refinery in Durrës, Albania, near Porto Romano. With a processing capacity of 150,000 barrels per day (BPD), this project will revolutionize Albania's

energy sector. Investors will have full management and control over spending, ensuring optimal utilization of their funds with complete transparency provided to the project owner, Oil Palmir JSC.

I. EXECUTIVE SUMMARY

Oil Palmir JSC is leading an ambitious investment to establish a state-of-the-art refinery in Albania, with an impressive processing capacity of 150,000 barrels per day (BPD). This initiative builds upon Albania's strategic location, abundant crude oil reserves, and emerging role as a regional energy player. The project is designed to address Albania's heavy reliance on imported fuels, meet growing regional demand, and position the country as a significant energy hub in the Balkans.

Key Objectives

1. **Maximizing Refinery Efficiency:** Achieving a processing depth exceeding 90%, significantly improving upon Albania's outdated refining infrastructure.
2. **Reducing Import Dependency:** Addressing Albania's current reliance on imported fuel by processing domestic and regional crude oil.
3. **Regional Energy Hub:** Establishing Albania as a pivotal player in the Balkan energy market through competitive pricing and eco-friendly production.
4. **Economic Growth:** Contributing to Albania's GDP while creating sustainable employment opportunities.

II. Company overview

Our company has registered under Statement No.15689, of 11.09.1996 of Tirana District Court, NIPT J63208448W with address: Lagja "29 Marsi" Patos, Fier, Albania has started its activity in the field of construction has its activity in this area by participating in several tenders initially accredited by the World Bank and several municipalities such as in : infrastructure, sewer, aqueduct, bridges, etc.

The Company "Palmir" has participated in several tenders for concreting and moving along of several dikes with the rivers Shkumbin dhe Vjosa.

We have qualified technical staff engineer with several years experiences.

Today our company has in use powerful machineries and plants for taking the major works such as: highways, squares, large construction objects and large more stories palaces. The Company has worked on the construction of the Levan – Vlore and Levan - Dames section of the Pan – European VII-th Road Corridor as subcontractor with a contract with company "Alpine Mayreder Bau GmbH" and with "Todini Construzioni Generali".

Palmir L.t.d has worked on the construction of the Levan – Vlore and Levan - Dames section of the Pan – European VII-th Road Corridor in production, transportation and placement of concrete RCK 150, RCK 200, RCK 250, RCK 300, RCK 350, RCK 400, RCK 450 (carried to summary 40.000 m3 concrete for“Alpine Mayreder Bau GmbH” and 10.000 m3 concrete for “Todini Construzioni Generali”).

On the quality of administrator **Mr. Perparim Gropa** is owner of “Oil Palmir”SH.A. The Company “Oil Palmir”SH.A with Head Office in Fier, Albania, with NIPT L23401403P, with main activities: extrusion, refining, trade with wholesale and retail of the hydrocarbons. The Company “Oil Palmir”, according to master plan drafted by experts of the field and on the basis of the Council of Ministers Decision No. 28 dated 10.05.2013 and License No.366/2 dated 11.07.2014. Construction of the refinery has received the approval of the Republic of Albania Ministry of Energy.

	REPUBLIKA E SHQIPËRISE MINISTRIA E EKONOMISË, TREGTISË DHE ENERGJITIKËS QENDRA KOMBËTARE E REGJISTRIMIT		NUMRI SERIAL: SN-172233-09-12
ÇERTIFIKATË REGJISTRIMI			
Personit të tatueshëm: OIL PALMIR – Shoqëri Anonime			
Statusi: Aktiv			
Me adresë kryesore: Fier, Patos, Lagjia 29 Marsi, Kilometri i 6 Fier-Patos			
I jepet ky numër identifikimi (NUIS): L23401403P			
Afati i veprimtarisë: Nga: 27/09/2012 deri			
DATA E REGJISTRIMIT 01/10/2012			
DATA E LËSHIMIT 02-10-2012			
SPORTELI I SHËRBIMIT:			
 QENDRA KOMBËTARE E REGJISTRIMIT <i>Haxhi Krasniqi</i> (Emri, Mbiemri) i nëpunësit të sportelit			
Kjo çertifikatë mbetet pronë e Qendrës Kombëtare të Regjistrimit dhe duhet të kthehet në rast se ka ndryshime të ndonjë detaji ose ndërprerjet detyrimi ligjor për të qenë person i tatueshëm.			

Republic of Albania
Ministry of Finance and Economy
National Business Centre

Serial Nr.SN-172233-09-12

QKB
National Business Center

Taxable Person
OIL PALMIR
Status – Active



Main address: Lagjja 29 Marsi, 6th km Fier-Patos

Is conferred the identification number (NUIS)

L23401403P

Term of activity: From 27-09-2012

Date of registration: 01-10-2012

Date of issue: 22.06.2023

Service desk

Name surname and signature of desk official

It is strictly forbidden to laminate this certificate

Digitally signed by National Business Centre

Date 22.06.2023



III. Market and industry analysis

III. 1 Location

Location: 9C8C+GR4, Rruga Punishte e Barutit, Durrës, Albania

Site Plan (200 Hectares) near Porto Romano



Map Legend:



Proposed area: 200 Hectares
Dimensions: 2.2Km x 0.9 Km



Porto Romano Area + Fuel Deposits

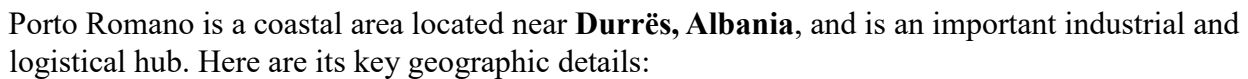


Shkozet - Porto Romano Road



Tirana - Durres Highway





- ### Nearby Infrastructure:

- ### Strategic Importance:

6





1. Administrative Division:

- **Country:** Albania
- **County:** Durrës County (**Qarku i Durrësit**)
- **Municipality:** Durrës Municipality
- **Administrative Unit:** Durrës

Porto Romano is an **industrial and port area** rather than a residential or commercial district. The zoning includes:

- 8

- **Residential and Commercial Areas** – Some small housing settlements and businesses exist, but the region is mainly industrial.

3. Nearby Settlements and Infrastructure:

- **Durrës City Center** (about 6 km southeast)
- **Shënavlash and Rrashbull** (small settlements inland)
- **SH2 Highway** (connects to **Tirana, 39 km away**)
- **Durrës Port** (major port for Albania)
- **Railway Connection** (Durrës-Tirana line) **Future Developments:**
- **New Porto Romano Deep-Sea Port** (to replace Durrës Port's cargo operations)
- **Oil Refinery and Energy Projects** (potential sites for industrial expansion)
- **Infrastructure Improvements** (roads, environmental restoration, and logistics hub expansion)

III.1.1 Traffic Interconnections of Porto Romano, Durrës, Albania

Porto Romano is strategically located along the Adriatic coast and is well-connected through multiple transport networks, including **road, rail, and maritime infrastructure**. Below are the key transportation interconnections:

1. Road Connections

- **SH2 Highway:** Connects Porto Romano to **Durrës (6 km southeast)** and **Tirana (39 km east)**, serving as Albania's primary corridor for trade and logistics.
- **SH85 Road:** Links Porto Romano directly to industrial zones and facilitates access to the planned **Porto Romano Deep-Sea Port**.
- **Durrës Bypass Road:** Helps divert traffic from urban areas to facilitate smoother logistics.

2. Rail Network

- **Durrës-Tirana Railway Line:**
 - The existing railway line runs from **Durrës to Tirana**, with connections to Porto Romano planned as part of Albania's railway modernization.
 - Future **rail extensions** may connect the **Porto Romano Free Zone** and the new port with national rail networks.

3. Maritime Transport

- **Porto Romano Deep-Sea Port (Under Development):**
 - A **new deep-sea port** is being constructed to **replace Durrës Port's cargo operations**.
 - It will include **dedicated terminals for fuel, LNG, and containerized cargo**.
 - The port will serve as a **regional hub** for shipping in the Adriatic and Mediterranean.
- **Durrës Port (Existing):**
 - Until Porto Romano Port is operational, Durrës Port remains Albania's **largest seaport**.
 - It handles bulk cargo, containers, and passenger ferries to Italy.

4. Air Transport

- **Tirana International Airport (TIA) – 35 km East** ◦ The nearest airport is **Tirana International Airport "Nënë Tereza" (TIA)**, accessible via SH2.
 - It serves **passenger and cargo flights**, supporting trade operations.

5. Future Developments

- **Integration of Porto Romano with Pan-European Transport Corridor VIII** (Italy – Albania – North Macedonia – Bulgaria).

- **Expansion of road and railway networks** to support increased cargo movement.
- **Enhanced intermodal transport** between sea, road, and rail for logistics efficiency.



SWOT Analysis

Strengths

Strategic Location Options – The refinery has two potential locations: **Fier**, near Albania's largest oil fields, and **Porto Romano, Durrës**, a key port city. Both options offer logistical advantages, ensuring cost-efficient crude supply and easy access to export markets.

Strong Market Potential – Albania and the Balkan region have a high demand for refined petroleum products, reducing reliance on imports and positioning the refinery as a key supplier.

Availability of clean fuels There are no available facilities in Albanian Ports concerning clean fuels. Durrës Port is currently envisaging to undertake the necessary studies to make available facilities on clean fuels in the actual port and in the same time in the new port in Porto Romano.

Cutting-Edge Technology – The refinery will use advanced, **EU-compliant** technology to produce **eco-friendly fuels (Euro 5 standard)**, ensuring efficiency, sustainability, and competitiveness.

Government Collaboration & Incentives – The option to acquire and redevelop **Porto Romano's infrastructure** aligns with Albania's economic strategy, potentially unlocking **government incentives** and policy support.

Attractive Financials & ROI – With a projected **payback period of 5 years**, an **NPV of €2-3 billion**, and an **IRR exceeding industry benchmarks**, the project presents a solid investment opportunity.

Job Creation & Economic Growth – The refinery will create **10,000 construction jobs** and **2,500 permanent jobs**, boosting local employment and contributing to Albania's **GDP growth**.

Weaknesses

High Initial Investment – The project requires **€3 billion** plus an optional **€600 million** for Porto Romano redevelopment, demanding **strong investor confidence** and financing.

Regulatory & Bureaucratic Hurdles – Large-scale industrial projects often face **delays in approvals, permits, and environmental assessments**, potentially affecting the construction timeline.

Dependence on Crude Oil Supply – The success of the refinery is reliant on **stable crude oil production from Albania and regional suppliers**, which could be impacted by fluctuations in production or pricing.

Infrastructure Gaps – While Porto Romano provides strong export access, Albania's **transport and pipeline network** may require additional upgrades to support large-scale refining operations.

Opportunities

Expansion into Regional Markets – The refinery can **export fuel** to high-demand markets in the **Balkans, EU, and Mediterranean region**, expanding its revenue streams.

Sustainable & Green Energy Integration – Leveraging **renewable energy solutions** (e.g., solar power for operations or biofuel production) could improve **ESG (Environmental, Social, Governance) ratings** and attract eco-conscious investors.

Public-Private Partnerships (PPP) – Collaboration with the **Albanian government** and **international investors** could unlock subsidies, tax breaks, and additional financing options.

Vertical Integration & Logistics Optimization – By acquiring the Porto Romano redevelopment, the project could **integrate logistics operations**, improving cost efficiency and supply chain control.

Potential for Petrochemical Diversification – Expansion into **petrochemical production** (plastics, chemicals, lubricants) could **diversify revenue sources** beyond fuel sales.

Threats

Market & Price Volatility – Fluctuations in **global crude oil prices** and **fuel demand** could impact profitability.

Geopolitical Risks – Albania’s proximity to politically sensitive regions may expose the project to external **geopolitical uncertainties** affecting oil supply and trade policies.

Environmental & Social Concerns – Refinery operations must comply with **strict environmental regulations**, and potential **public opposition** to industrial expansion could lead to legal or reputational challenges.

Competition from Regional Refineries – Competing refineries in **Greece, Italy, and Turkey** may leverage established supply chains and economies of scale to maintain a competitive edge.

Delays in Project Execution – Unforeseen **construction challenges, labor shortages, or financial constraints** could extend the **project timeline** and increase costs.

IV. Investment & Financial Projections

1. Total Investment & Fund Utilization

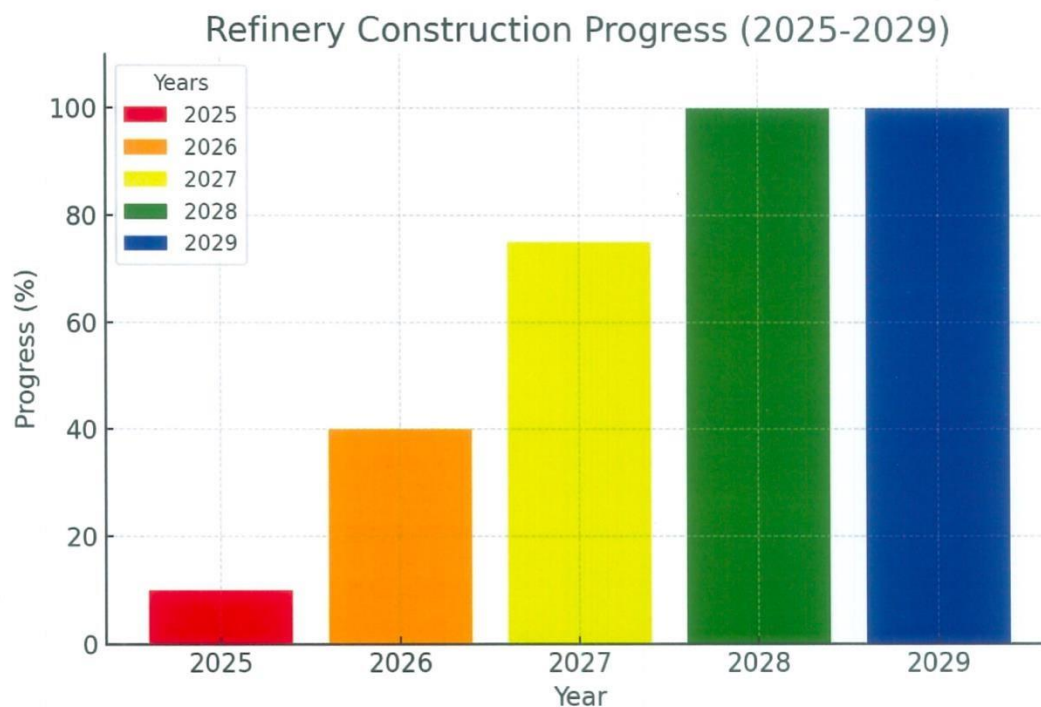
Investment Component	Cost (in USD)
Land Acquisition & Permits	50 million
Engineering & Design	300 million
Construction & Infrastructure	1.5 billion
Refining Equipment & Installation	850 million
Renewable Energy & Hydrogen Facility	350 million
Logistics & Transport Network	150 million
Compliance, Safety & Environmental Protection	100 million
Miscellaneous & Contingency	100 million
Total Investment	3.3 billion

- **Investor Rights & Control:**

- Full authority over financial management & fund allocation
- Direct procurement & contractor selection
- Real-time financial reporting and auditing available to Oil Palmir JSC
- Commitment to transparency and compliance with international financial regulations

2. Revenue & Profitability Forecast

Year	Production (BPD)	Revenue (USD)	Profit (USD)
1	100,000	4.2 billion	700 million
2	125,000	5.1 billion	950 million
3	150,000	6.2 billion	1.2 billion



4 150,000 6.5 billion 1.4 billion

5 150,000 6.8 billion 1.6 billion

- **Projected ROI: 4-6 years**
- **Future Expansion Potential:** Scale-up capacity by 30% after year 5

Market & Competitive Advantage

1. Global & Regional Market Demand

- **Albania's Current Import Dependency:** 90% of refined oil is imported
- **Regional Market Access:** High demand in Kosovo, Montenegro, North Macedonia, Greece, and Italy
- **Global Trade Opportunities:** Direct distribution via Rotterdam (Europe) and Singapore (Asia)

2. Key Competitive Advantages

- **State-of-the-Art Refining Technology:** Ensures higher yields & reduced emissions
- **Exclusive Control Over Operational Strategy:** Investors manage all major decisions
- **Guaranteed Market Share:** Secured buyer agreements & government contracts
- **Renewable Energy & Hydrogen Integration:** Adds revenue diversification & ecompliance

Governance & Transparency

- **Investor-Led Decision Making:** All strategic and financial decisions under investor control

- **Auditable Financial Management:** Transparent reporting structure to Oil Palmir JSC
- **Regulatory Compliance:** Adheres to EU & global energy market standards
- **Risk Mitigation:** Insurance coverage and contingency planning for all operations

Environmental & Social Responsibility

- **Zero Pollution Action Plan:** Comprehensive environmental protection initiatives
- **Carbon Capture Technology:** Eliminates greenhouse gas emissions • **Sustainable Energy Utilization:** Integration of solar, wind, and hydropower • **Social Commitment:**
 - Annual Reforestation of 1 million trees
 - Local Employment & Training Programs
 - Infrastructure Development in Host Communities

Next Steps & Project Timeline

Implementation Phases

Phase	Duration	Key Milestones
Land Acquisition & Permitting	6 months	Site secured; legal approvals obtained
Engineering & Design	12 months	Detailed blueprints, safety & compliance approvals
Construction & Infrastructure	24 months	Foundation, processing units, & logistics network built
Equipment Procurement & Installation	12 months	Installation & systems integration
Testing & Commissioning	6 months	Safety testing, operational fine-tuning
Full Commercial Operation	Year 3	150,000 BPD refinery operational

Maps & Visuals

1. Strategic Location & Logistics Maps



SOUTHEAST EUROPE



ALBANIA





CORIDOR 8 BARI - VARN

Porto Romano is situated on Albania's Adriatic coast, approximately 80 km from Italy across the sea and 300 km from Greece. It is integrated into Pan-European Corridor VIII, a major transport route connecting the Adriatic to the Black Sea via Durrës, Tirana, Skopje, Sofia, and Varna. This corridor enhances access to key markets in the Balkans, Central Europe, and beyond.

Albania is a member of the Pan-European Corridor system. The Pan-European Corridor VIII starts from the port of Durrës on the Adriatic Sea in the west of Albania, continues East across Albania; joins the Republic of North Macedonia on the north of Ohrid lake and after joining Skopje continues to Bulgaria. It ends at Varna / Burgas at the Black Sea in the east. The Port of Durrës serves as the Corridor VIII West Gate linking Albania, with Italy and securing flawless access through Puglia ports in Italy to the existing Scandinavian – Mediterranean corridor and to the newly planned Baltic Sea – Adriatic Sea Corridor. Through the Port of Durrës, Corridor VIII closes the connections between Three Seas: North Sea, Mediterranean Sea and Black Sea. On the regional scale, the Port of Durrës is the main gate of the goods and passengers imported/exported for Kosovo and North Macedonia. Port of Durrës is also an important part of the Adriatic and Ionian Highway. While missing from the new draft TEN-T regulation

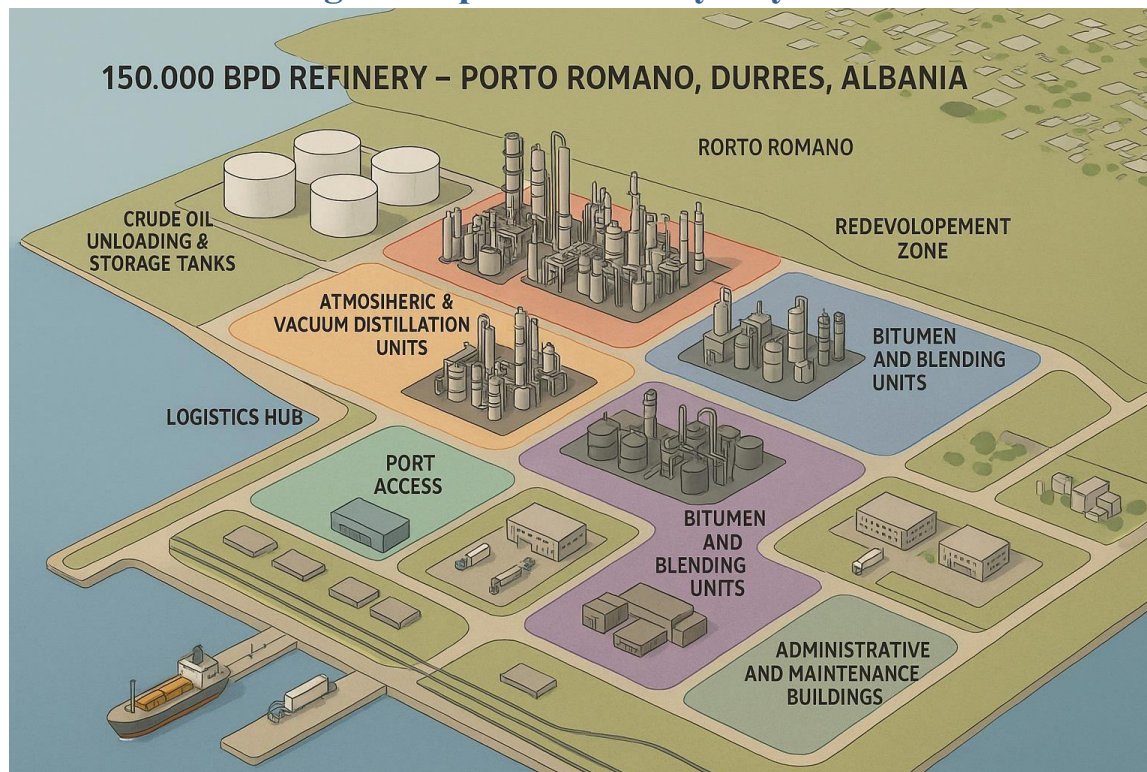
of 2021, the Adriatic-Ionian Highway stretches for 1,550 km along the coast of the Adriatic and Ionian Seas, from Trieste in Italy to Kalamata in Greece.

2. Refinery Layout & Facilities

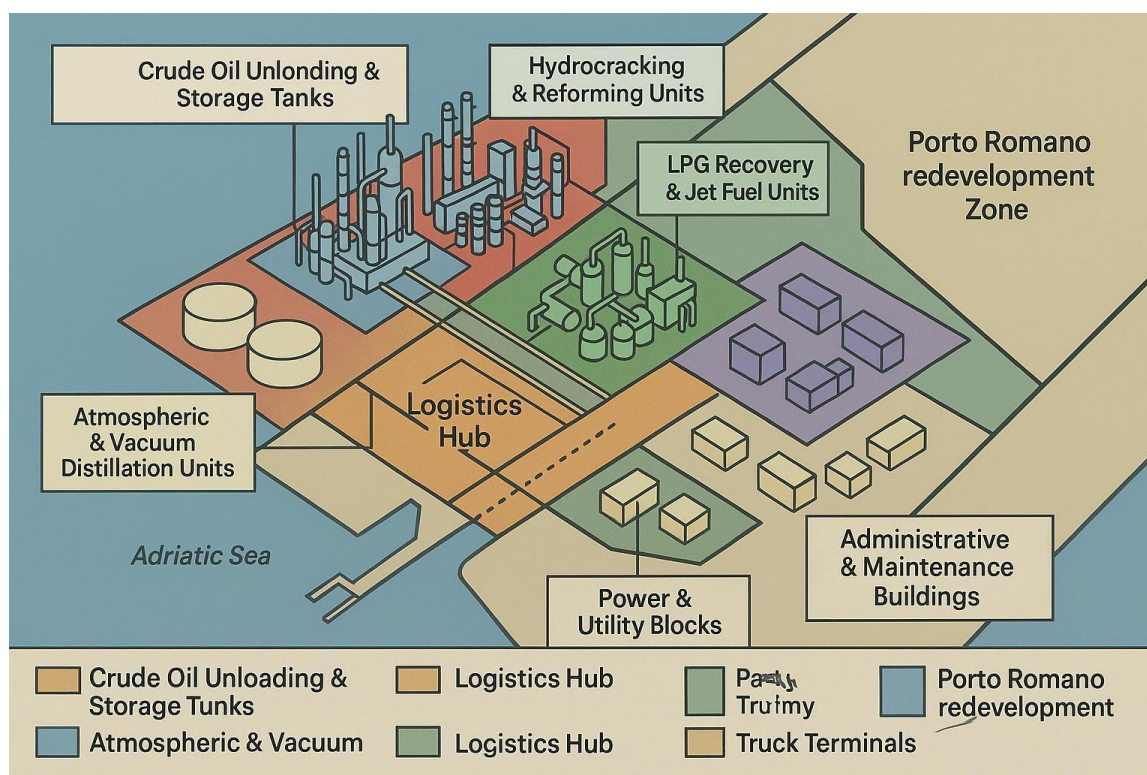
Porto Romano Refinery – Concept Masterplan

150,000 BPD Integrated Refinery | Porto Romano, Durrës, Albania

Realistic Rendering of Proposed Refinery Layout



Engineering-Style Schematic Layout (Color-Coded Zones)



Zone-by-Zone Visual Summary

Crude Oil Unloading & Storage

Positioned along the waterfront to allow direct offloading from tankers. Large-capacity tanks ensure stable supply buffering and gravity-fed flow into primary distillation.

Atmospheric & Vacuum Distillation

Core of the refinery. Separates crude into fractions based on boiling point under varying pressures — feeding downstream units efficiently.

Hydrocracking & Reforming

Converts heavier fractions into lighter, high-value fuels. These units boost jet fuel, diesel, and gasoline yields. Centrally located for optimal integration.

LPG & Jet Fuel Recovery

Refined streams undergo gas separation and recovery, generating LPG and aviation-grade jet fuel. Located near transport links for rapid dispatch.

Bitumen & Blending

Produces asphalt and road-grade bitumen. Includes tanks and blending skids. Tucked in the south sector for easy loadout and thermal handling.

Waste Treatment & Emissions

Environmental control zone. Houses water treatment, flare stacks, and emissions scrubbers. Isolated downwind from main admin and urban edges.

Power & Utility Blocks

Provides steam, electricity, cooling water, and air. Located centrally to feed processing and storage zones efficiently.

Logistics Hub

Multi-modal access via port, railway, and trucks. Critical for product dispatch and material inflow. Interfaces with Albania's transport network.

Admin & Maintenance

Includes control rooms, offices, fire safety, and workshops. Located at the site entrance with green buffer zones toward the redevelopment area.

Porto Romano Redevelopment Zone

Strategically aligned with national infrastructure and energy transition goals. Connects with broader Durrës Free Zone and logistics corridor.

Refinery Capacity & Cutting-Edge Technology

- **Processing Capacity:** 150,000 BPD
- **Annual Throughput:** Approx. 55 million barrels • **Advanced Processing Units:**
 - Atmospheric & Vacuum Distillation
 - Catalytic Reforming & Isomerization
 - Hydrocracking & Desulfurization
 - Green & Blue Hydrogen Production
 - Carbon Capture & Storage (CCS) System
 - Renewable Energy Integration (Solar, Wind, Hydropower)
- **Projected Operational Lifespan:** 50+ years with routine upgrade

3. Supply Chain & Export Routes

Crude Oil Sourcing:

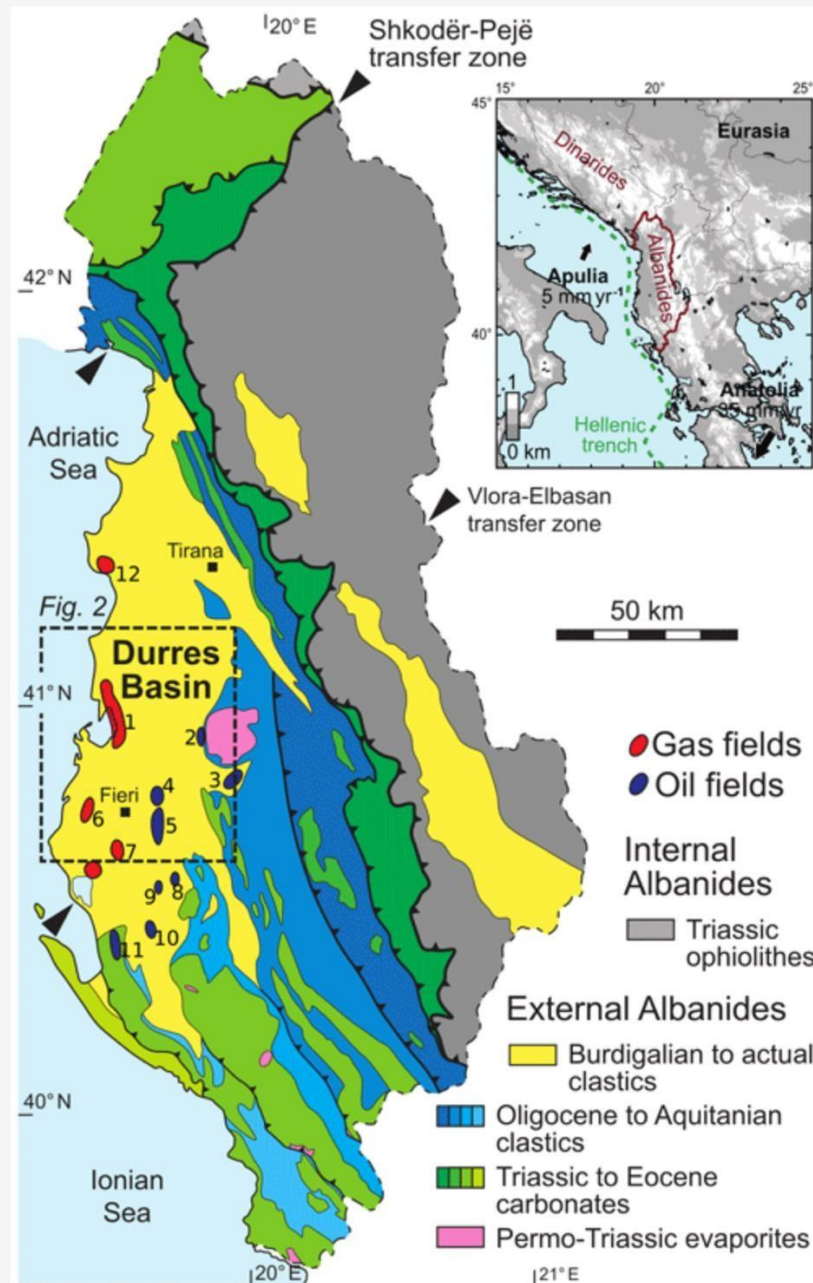
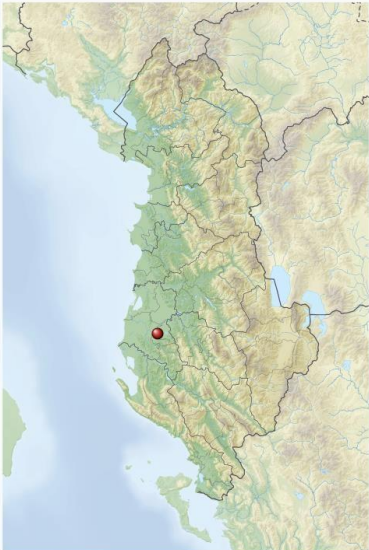


Figure 1 Simplified geological map of Albania. Oil and gas main fields are indicated in blue and red, respectively, and numbered: (1) Ballaj-Divjaka, (2) Pekishti, (3) Kucova, (4) Bubullima, (5) Patos-Marinza, (6) Seman-Poveica, (7) Frakula, (8) Balshi, (9) Cakrani, (10) Gorishti-Koculi, (11) Drashovice, and (12) Durrës. Dashed rectangle is the study area as plotted in Fig. 2. Upper right inset shows the geographical location of Albania and regional kinematics with respect to stable Eurasia (Métrois et al., 2015).

Patos-Marinëz Oil Field (central Albania): The largest onshore oil field in Europe, connected via a **dedicated underground pipeline** (approx. 50 km) directly to the refinery. **Patos-Marinëz** is an Albanian oil field that was discovered in 1928 and became operational in 1930. It is the biggest on-shore oil field in Europe, and with its 11,854 barrels (1,884.6 m³) per day the biggest oil producing field in Albania. The Patos Marinëz oil field is located 10 kilometres (6 mi) east of

the city of Fier in south central Albania. Its proven reserves are about 2 billion barrels ($320 \times 10^6 \text{ m}^3$). Patos Marinëz has only heavy oil and is in production since the 1930s.

Patos Marinëz	
	
Location of Patos Marinëz	
Country	Albania
Region	Fier County
Location	Patos
Block	Patos-Marinëz
Offshore/onshore	Onshore
Coordinates	
Operator	Bankers Petroleum, Albpetrol
Field history	
Discovery	1928/ Ina
Start of production	2004 ^[1]
Production	
Current production of oil	medium-heavy oil t/a (12.556 bbl/d or 1.9962 m ³ /d)
Estimated oil in place	1.500 million barrels ($\sim 2.046 \times 10^5 \text{ t}$)
Producing formations	sandstone

Production and Reserves

Table 2: Reserves of Patos-Marinza Oil Field

Fuel description	Reserves classification	Quantity	Units	Data year	Source
crude oil and condensate	Remaining recoverable reserves	29.04	million bbl	2021	[1]
oil	Remaining recoverable reserves	18.42	million bbl	2018	[9]
oil	intial recoverable reserves	206.94	million bbl	2018	[9]

million bbl = million barrels of oil

Table 3: Production from Patos-Marinza Oil Field

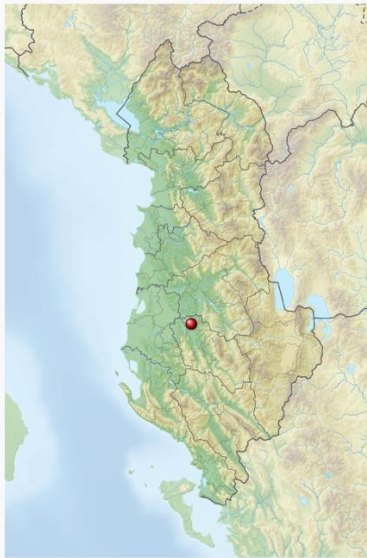
Category	Fuel description	Quantity	Units	Data year	Source
cumulative production	oil	188.52	million bbl	2018	[9]
production	crude oil and condensate	8.88	million bbl/y	2014	[1]
production	oil	5.5	million bbl/y	2019	[10]
production	oil	5.89	million bbl/y	2019	[11]
production	oil	7.52	million bbl/y	2015	[11]
production	oil	6.13	million bbl/y	2016	[11]
production	oil	5.56	million bbl/y	2017	[11]
production	oil	5.28	million bbl/y	2018	[11]
production	oil	4.48	million bbl/y	2020	[11]

million bbl/y = million barrels of oil per year

million bbl = million barrels of oil

Kuçovë Oil Field (south-central Albania): Linked via an **intermediate pipeline network** that merges with the Patos pipeline before reaching Porto Romano. **Kuçova oil field** is an Albanian oil field that was discovered in 1928. It is the second biggest on-shore oil field of Albania, after the Patos-Marinza Oil Field. The Kuçova oil field is located near the town of Kuçovë, 30 kilometres (19 mi) east of the city of Fier in south central Albania. Its proven reserves are about 490 million barrels ($78 \times 10^6 \text{ m}^3$)

Kuçova oil field



Location of Kuçova oil field

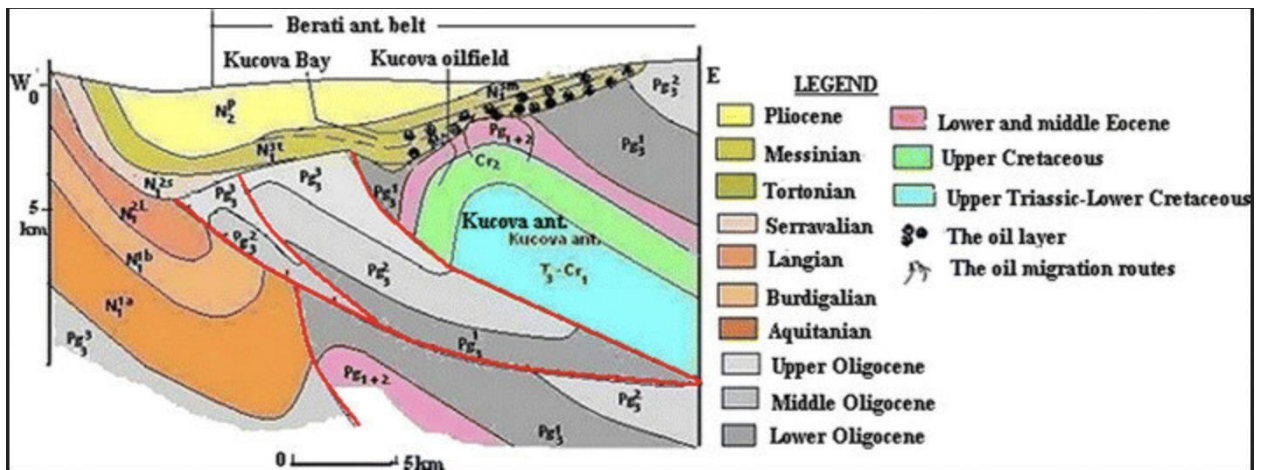
Country	Albania
Region	Berat County
Location	Kuçovë
Offshore/onshore	Onshore
Coordinates	 40.82°N 19.92°E
Operators	Albpetrol
Partners	Sherwood

Field history

Discovery	1928
Start of production	2004

Production

Current production of oil	1,000 barrels per day (~50,000 t/a)
Estimated oil in place	1,000 million barrels (~ 1.4×10^8 t)



The schematic geological cross-section in Kucova Oilfield



Crude Transportation Route:

TEST REPORT N. GE16-0014.001

Date: March 01, 2016 Pag. 1 of 9

Sample of : CRUDE OIL
Received on the : 30/12/2015
Client : BANKERS
Sample Conditions : Metal tin
Label Description : "Patos Marinza Sales Oil"

Rif. Lab. : 0014.001

TEST RESULTS

CRUDE OIL CHARACTERISTICS

Methods	Tests	M. Units	Results
ASTM D 1298	DENSITY AT 15°C	kg/m ³	999.6
CALC	API GRAVITY AT 60°F	Nr	9.97
ASTM D 4294	SULPHUR CONTENT	% m/m	5.702
UOP 163	SULPHUR MERCAPTANS	mg/Kg	624
UOP 163	H ₂ S	mg/Kg	<1
ASTMD 4629	TOTAL NITROGEN	mg/Kg	1650
ASTM D-4530	MICRO CONRADSON CARBON	% m/m	17.21
ASTM D323	REID VAPOUR PRESSURE	Kpa	11.72
ASTM D-5853	POUR POINT	°C	+3
ASTM D-445	VISCOSITY AT 25°C	mm ² /s	9534
ASTM D-445	VISCOSITY AT 50°C	mm ² /s	1029
UOP 375	UOP K FACTOR	Nr	11.2
ASTM D 664	TOTAL ACID NUMBER	mgKOH/gr	0.772
BP 237	WAX	% m/m	0.16
ASTM D7691	NICKEL	mg/Kg	80
ASTM D7691	VANADIUM	mg/Kg	621
ASTM D7623	MERCURY	mg/Kg	<1
IP 143	ASPHALTENES	% m/m	13.51
ISO 6245	ASH	% m/m	0.071
IP 77	SALT CONTENT	mgNaCl/l	250
ASTM D4006	WATER	% m/m	1.80
ASTM D4007	S&W	% v/v	2.10
ASTM D-93	FLASH POINT	°C	32

The Responsible

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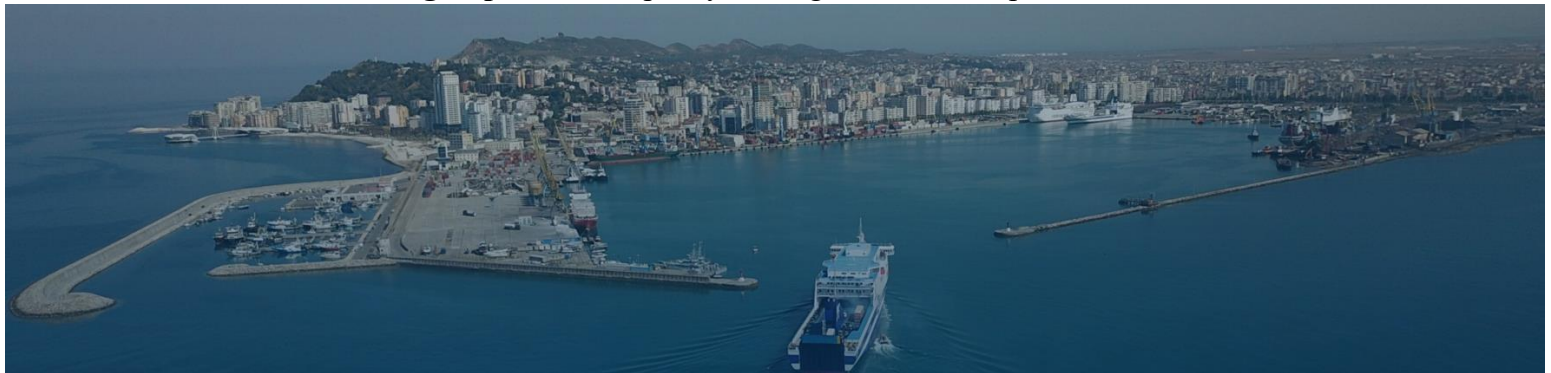
Membri del gruppo SGS

Sede Legale: Milano - Via G. Gozzi 1/A - Cap. Soc. € 2.500.000 i.v. - C.F. 01.000.000.000 - P. IVA n. 01705020155
REA MI n. 1402706 - Cod. Min. n. M220145 - Società unipersonale soggetta a direzione e coordinamento di SGS S.p.A. Italy

- Pipelines transport crude oil from Patos-Marinëz and Kuçovë directly to the **refinery at Porto Romano**, minimizing trucking and reducing transport emissions and costs.

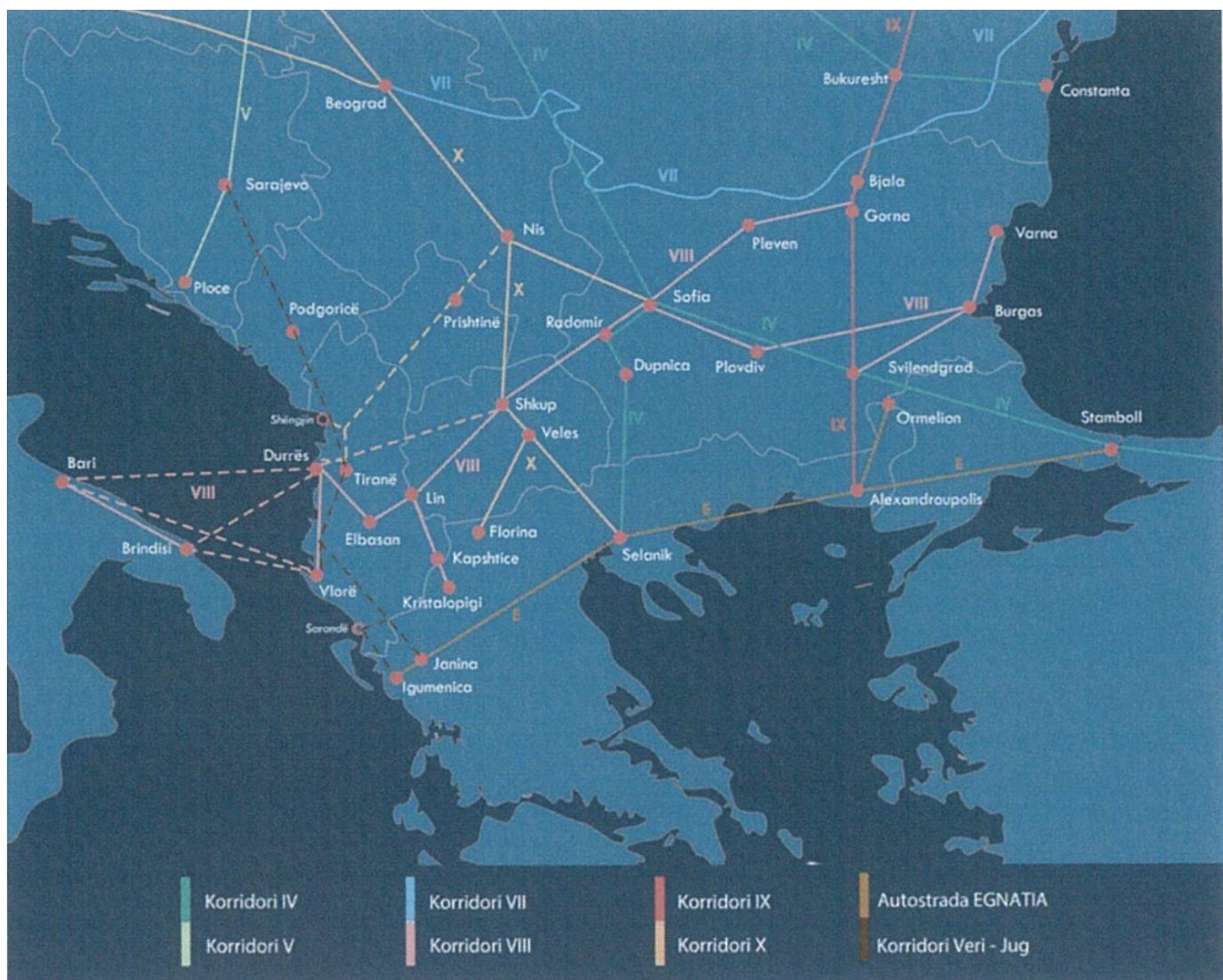
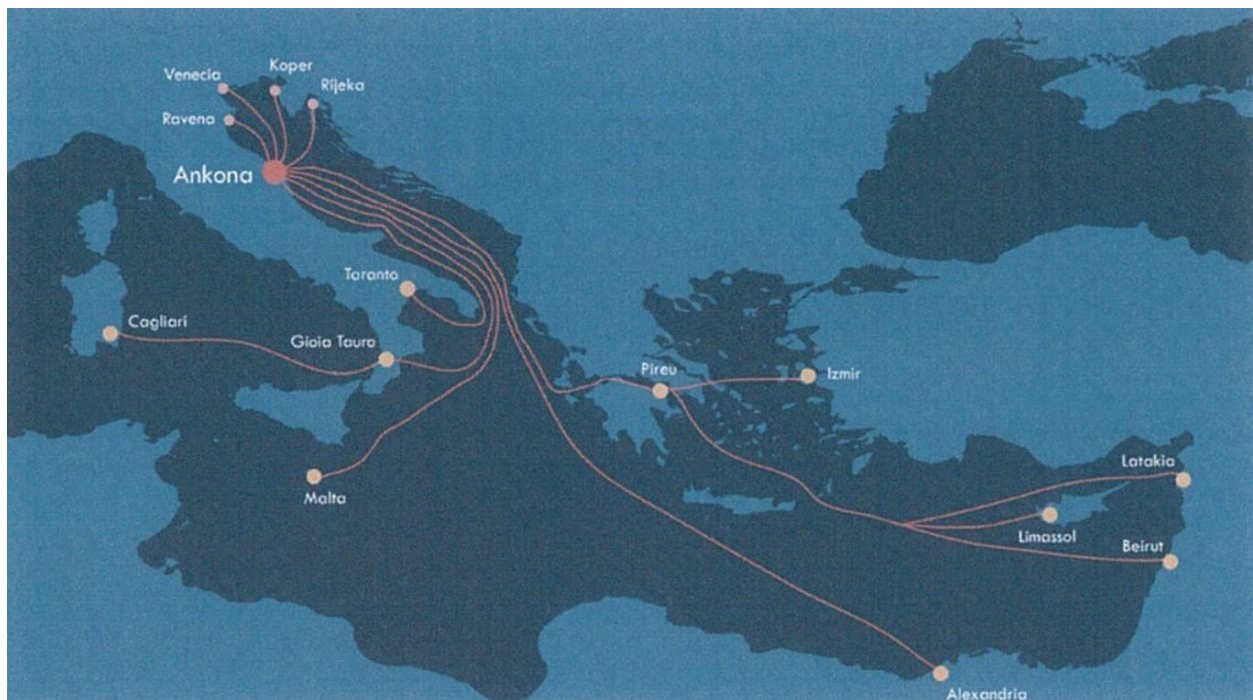
Refinery Location:

- **Porto Romano, Durrës:** Located on the **Adriatic coast**, part of Durrës city, home to Albania's **largest port** with capacity for large-scale fuel exports.



Product Distribution Routes:

- **Marine Export:** Refined fuels (gasoline, diesel, jet fuel, LPG, bitumen) are shipped via the **Port of Durrës to Italy, Greece, Croatia, and Mediterranean markets.**
- The marine export waterway from Port of Durrës (Albania) facilitates shipping to Italy, Greece, Croatia, and other Mediterranean markets. This route leverages the Adriatic Sea as a key link in the Western Balkan Transport Corridor, part of the broader European TEN-T network, which aims to improve connectivity within the region. The Adriatic Sea



9 EUROPEAN TRANSPORT CORRIDORS

Integrating:

- Core Network Corridors
- Rail Freight Corridors

Corridors consist of railways, roads, inland waterways, ports, airports and rail-road terminals. They ensure coherence in network development, avoiding duplication and increasing synergies between infrastructure planning and operational needs.



Support Infrastructure:

- **Storage Tanks:** Near the refinery and port for both crude oil and refined products.
- **Power Substation:** On-site facility powered by grid and backup generators.
- **Waste Management Plant:** Handles effluents and emissions in line with EU standards.

Conclusion & Investor Opportunity

This refinery will position Albania as a major energy hub in the Balkans while ensuring longterm profitability for investors. With a total investment of **3.3 billion USD**, this project will generate over **6.8 billion USD in annual revenue** and achieve full ROI within **4-6 years**. Investors will have **full management control**, ensuring the most efficient and transparent allocation of funds. Oil Palmir JSC welcomes investors to lead this landmark energy project with complete transparency, high profitability, and long-term sustainability.

TEST

01,

APPENDICES

APPENDIX A - SGS TEST



16153 Tel.: Fax:

011, Via

REPORT Ne GEI 6-00140001

Date: 2016 Pag. 1 of 9

Sample of : CRUDE OIL

Received on the .. 30/12/2015

Rif. Labe : **0014.**

Client • BANKERS

Sample Conditions Metal tin

Label Description : "Patos Marinza Sales Oil"

TEST RESULTS

CRUDE OIL CHARACTERISTICS

Methods	Tests	M. Units	Results
ASTM D 1298	DENSITY AT 15 °C	kg/m	999.6
CALC	API GRAVITY AT 60 °F	Nr	9.97

jurisdiction

alteration.

TEST

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ASTM D 4294	SULPHUR CONTENT	% m/m	5.702
UOP 163	SULPHUR MERCAPTANS	mg/l<g	624
UOP 163	1-12S	mg/Kg	
ASTMD 4629	TOTAL NITROGEN	mg/Kg	1650
ASTM D-4530	MICRO CONRADSON CARBON	% m/m	17.21
ASTM D323	RED VAPOUR PRESSURE	l<pa	11.72

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ASTM D-5853	POUR POINT		+3
ASTM D-445	VISCOSITY AT 25 °C	mm ² /s	9534
ASTM D-445	VISCOSITY AT 50 °C	mm ² /s	1029
UOP 375	UOP FACTOR	Nr	11.2
ASTM D 664	TOTAL ACID NUMBER	mgKOH/gr	0.772
BP 237	VVAX	% m/m	0.16
ASTM D7691	NICKEL	mg/Kg	80
ASTM D7691	VANADIUM	mg/Kg	621
ASTM D7623	MERCURY	mg/l<g	
IP 143	ASPHALTENES	% m/m	13.51
ISO 6245	ASH	% m/m	0.071
IP 77	SALT CONTENT	mgNaCl/l	250
ASTM D4006	WATER	% m/m	1.80
ASTM D4007		% v/v	2.10
ASTM D-93	FLASH POINT		32

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REPORT GE16-00Un001 Date, March 2016, 2016 pag. 4 of 9

METHODS	YIELD		5-70	70-165	90
	At Tel Quel	% m/m	0.09	3.48	
	At Tel Quel	% vol.	C). 14	4.77	.50
ASTM D	TEST	M.U.			

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4052	Dens.	l/g/m ³	677.3	760.9	806.6
1250	API GRAVITY AT GO °F		77.4	54.4	43.8
4294	Total Sulphur	% m/m	0.21	0.49	1.04
UOP 163	Sulphur Mercaptans	mg/Kg	963	295	59
4629	Total Nitrogen	mg/Kg			
323	Raid Vapor Pressure	l/Pa	14.9	9.7	1.1
6839	Paraffins	% v/v	33.38	16.31	8.62
6839	Iso-Paraffins	% v/v	45.93	35.94	43.68
6839	Naphthenes	% v/v	19.73	31.10	25.40
6839	Aromatics	% v/v	0.96	16.65	22.30
97	Pour Point				
2500	Cloud Point				
2386	Freezing Point				<-68
4737	Cetane Index	num	27.3	23.4	34.2
1500	Colour	num	0		0
445	Viscosity at 37.8 °C	mm ² /s	N.A.	0.742	1.08i
445	Viscosity at 50 °C	mm ² /s	N.A.	0.633	0.905
1322	Smoke point	mm	N.A.	30	21.5
ISO 2160	Copper Strip Corrosion		N.A.		
4929	Organic Chlorides	mg/kg			
1840	Naphthalenes	% v/v	<0.01	0.03	0.15
93	Flash Point				50

hours @ 50 °C

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REPORT GE16-0014E001

Date: March 2016, 2016 Page 5 of 9

METHODS	YELD		190-230	230-325	325-370
	At Tel Quel	% m/m	3.22	7.45	6.94
	At Tel Quel	% vol.	4.03	8.42	7.45
ASTM D	TEST				
4052	Dens. i5 °C	Kg/m3	832.9	884.4	931.3
1250	API Gravity AT GO °F	Nr	38.3	28.4	20,4
4294	Total Sul hur	% m/m	1.48	2.49	3.41
[JOP 163	Sul hur Merca tans	mg/l<g	40	58	135
4629	Total Nitro en	mg/Kg		191	496

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(JOP 269	Basic nitrogen	pm		42	94
97	Pour Point		<-36		-24
UNI EN	CFPP				N.A.

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2500	Cloud Point			<-36	-19
2386	Freezing Point			-41	-15
4737	Cetane Index	num	35.8	36.5	39.6
UOP 375	LJOP K FACTOR			11.2	
1500	Colour	num		LO.5	
445	Visc a 40 °c	mm2/s	1.419	3.105	10.32
445	Visc a 80 °C	mm2/s	0.840	1.535	3.569
1322	Smoke oint	mm	18	N.A.	N.A.
ISO 2160	Co er Stri Corrosion				
611	Aniline Point		46.8	45.8	43.0
EN 12916	Aromatics	% m/m	30.38	40.98	59.74
4929	Organic Chlorides	mg/kg			
4530	Micro CCH	% m/rn	<0.10	<0.10	<0.10
664	Total acid number	mg 1<01-1/gr	0.414	0.862	2.386
1218	Refractive Index@20 ° C	nD20		1.4882	1.5154
1840	Na thalenes	% v/v	1.21	8.24	19.45
BP 237	Wax	% m/m			
93	Flash Point		66	108	164

*2hours @ 100 °C; hours @ 50 °C

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TEST REPORT No **GE16-0014.001** Date: March 01, 2016 Page 6 of 9

METHODS	MELD		370-550
	At Tel Quel	% m/m	27.58
	At Tel Quel	% vol.	27.75
ASTM D	TEST		
4052	Dens.	Kg/m3	993.5
1250	API Gravity AT GO °F		10.8
4294	Total Sul hur	% m/m	4.81
UOP 163	Sulphur Mercaptans	mg/Kg	84
4629	Total Nitrogen	mg/Kg	1450
I-JOP 269	Basic nitrogen	mg/Kg	327
	Pour Point		+6
[JOP 375	(JOP K Factor	Nr	11.2
445	Visc a 40 °C	mm2/s	908.1
445	Visc a 100 °C	mm2/s	25.91
611	Aniline Point		51.6
4530	Micro CCH	% m/m	-1.45
664	Total acid number	mg	0.96
1218	Refractive Index@20 °C	nD20	N.A.*
BF) 237	Wax	% m/m	0.84
501	Nickel	mg/l<g	
IF) 501	Vanadium	mg/Kg	

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501	Sodium	mg/Kg	
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*Sample Too Dark

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METHODS	YELL)		370+	550+
	At Tel Quel	% ITI/m	77.51	49.93
	At Tel Quel	% vol.	73.40	45.65
ASTM D	TEST	M.IJ.		
4052	Dens.	Kg/m3	1055.5	1093.2
1250	API Gravity AT GO oF	Nr	2.5	-2.1
4294	Total Sul hur	% m/m	6.71	7.77
5291	Total Nitrogen	% m/m	0.49	0.57
I-JOP 269	Basic nitrogen	mg/Kg	997	1289
97	Pour Point		72	93
UOP 375	(JOP K Factor	Nr	-11.1	N.A.
445	Visc a 800	mm2/s	23613	14351410
445	Visc a loo °c	mm2/s	4013	1036745
445	Visc a 135 °C	mm2/s	425.7	34216
4530	Micro CCR	% m/m	22.65	34.95
664	Total acid number	mg KOH/gr	0.70	0.50
BP 237	Wax	% m/m	0.81	0.31
IP 501	Nickel	mg/Kg	103	
IP 501	Vanadium	mg/Kg	808	1249

IP 501	Sodium	mg/Kg	27	
36	Softening Point		47.4	105.0
5	Penetration 25 °c	Dmm	34.3	
143	As halthenes	% m/m	17.56	27.35
482	Ash content	% m/m	0.104	0.169

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Date: March 01, 2016 Page 8 of g

METODS	YELD	M.IJ.	C5-70	70-165	i 65-190	190-230	230-325	325-370
	At Tel Quel	% m/m	0.09	3.48	1.16	3.22	7.45	6.94

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	At Tel Quel	% vol.	0.14	4.77	1.50	4.03	8.42	7.45
ASTM D	TEST							
86	Distill, IBP		22	77	170	194	239	324
	5 % vol.		28	82	174	199	252	333
			34	86	177	201	255	340
	20%		37	98	-178	204	258	
	30%		39	109	179	206	261	347
	40%		41	115	•180	209	264	350
	50%		42	119		212	269	352
			45	122	182	215	273	354
			47	126	183	218	279	357
			51	134	184	220	284	360
			56	148	186	222	292	363
	95%		62	152	188	225	299	365
	FBI)		67	159	192	228	309	368

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Date: March 01, 2016 Pag, 2 of 9

FRACTIONED DISTILLA

ASTM D 2892	TBP Distillation	% mass	% vol.	Density at 15 °C Kg m ^s
	Fraction GAS	0.15	0.29	565.2 (i)
	05	0.09	0.14	677.3 (2)
	70	3.48	4.77	760.9 (3)
	165 - 190 °0	1.16	1.50	806.6 (3)
	190 - 230 °C	3.22	4.03	832.9 (3)
	230 - 325 °0	7.45	8.42	884.4 (3)
	325 370 °0	6.94	7.45	931.3 (3)
	370 °0 +	77.51	73.40	1055.5(3)

1 Calculated from ASTM D 2163

(2) Calculated from ASTM D 5134

(3) ASTM D 4052

ASTM D 5236	POT STILL Distillation	% mass	% vol.	Density at 15 °C Kg/m ³
	3700-55000	27.58	27.75	993.5 (3)

	550 °C +	49.93	45.65	1093.2 (3)
--	----------	-------	-------	------------

(3) ASTM D 4052

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APPENDIX B - LABORATORY TEST REPORT

Intertek Caleb Brett

Your Ref. : 3445

Date : 10-Sep-03

Laboratory Test Report No. 03-004386-0-ABDN

DESCRIPTION

LAB REF

Laboratory Report 03-004386-0-ABDN Page of

Patos Marinza Oil Field 18/7/03 Pad - D Tank 41 Tank Level 251.2m3

001-00

002-00

003-00**FOR THE**

C5-70 Deg C

- 165 Deg C 004-00**ATTENTION**

- 190 Deg C 005-00

006-00**OF -**

230 Deg C :

- 325 Deg C 007-00

- 370 Deg C 008-00SAMPLE

- 521 Deg C 009-00DETAILS

Deg C + Residue

011-00

Deg C + Residue

013-00SOURCE

Anglo Albanian Petroluem Ltd (AAP)

Mr M Porter

Operations Base

1 Samples received on 19-Aug-03

Patos

Anglo Albanian Petroluem Ltd (AAP)

CONTAINERS

x 5 Ltr Metal Cans

S

SEE ATTACHED

RESULTS

SHEETS

**E
A
L
S**

Tests marked With an asterisk(*) in this report are not included in the UKAS accreditation

(Or our laboratory)

(TOTAL NUMBER OF PAGES 11)

Reported by: _____ Approved by: Michelle Thomson - Analyst
Alistair Park Senior Chemist

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Intertek Caleb Brett

Wellheads Crescent, Wellheads Industrial Estate, Dyce, Aberdeen, AB21 7GA
Telephone No 01224 723242 Fax No 01224 722894

1 1

Notes on obtaining the Patos•Marinza crude oil sample

Refer to Anglo Albanian Petroleum report "First Production Phase (FPP) Export: Assay Sampling Report' dated 23 August 2003 for full details on sampling methodology, including photographs and schematics.

The date of sampling was Friday 18-July-2003 and injection of Solar diluent into the wells was stopped on Friday 11-July-2003 ("Solar" is a locally refined product, similar to automotive diesel). The sample production period was 6 days (12 to 17 July). Following the sample production period, there was a further day of nil production into the tank (Friday 18-July) to give additional residence time to promote good sand/water separation. The assay samples were taken during this final day of nil production into the tank.

Demulsifier chemical is used in Patos-Marinza oil production. The chemical used is Baker Petro*ite Separol DMO 85394 and typical dosage rate is 100 150 ppm in the net oil volume (i.e. without sand and water). The crude oil sample was taken from Tank No. 41 on wellpad D. The tank contents were at a temperature of 82 °C when the sample was taken.

Tank No. 41 is a direct-fired 2nd stage atmospheric treating tank where heat and residence time is used to treat the crude oil. Nominal tank capacity is 320 (—2,000 bbls). Heat is used (1) to reduce the viscosity of the oil and thereby improve sand settlement, and (2) to increase the density difference between the oil and water phases and thereby improve oil-water separation. Gas from the tank is either vented to atmosphere or recovered by a Vapour Recovery Unit (VRU) for use as fuel gas.

Crude oil enters Tank No. 41 on wellpad D by two methods:

- * directly from Tank No. 31 on wellpad D (which is a direct-fired 1st stage atmospheric treating tank), and
- * via tank truck from wellpad H and the five individual well sites (where the oil will have already received initial tank treating)

The approximate amount of oil processed in Tank No. 41 from each production location during the sample production period was as follows:

- * From Pad D: 233.6 m³ (1 bbls) or 37.0 %
- * From Pad H: 1 531 m³ (962 bbls) or 24.3 % * From single well sites; 244.0 m³ (1,535 bbls) or 38.7 %

and individual well production volumes are not measured with high accuracy. From the figures above, estimated total production during the sample period was 630.6 m³ (—4,000 bbls).

Considering the starting tank inventory and the tank capacity of only 320 m³ it can be seen that it was necessary to pump out some volume from the tank during the sample production period (to sales oil storage Tank No. 43) in order to prevent over-filling the tank.

Patos-Marinza oil production wells employ artificial lift using downhole Progressing Cavity (PC) pumps. Light oil is routinely used as required as downhole loading fluid to maintain good pumping conditions. Light oil used is crude oil from well M-976 (Marinza 2 layer) and is therefore highly compatible with crude oil from the other main layers (Upper Drizar Lower Driza, Marinza 1). From our records of light oil usage at these wells during the sample production period, we estimate that overall light oil content in the sample is around 5%. wellpad D by the addition of Solar diluent. This diluent addition is necessary to reduce viscosity for transportation in Albpetrol's pipeline to the refinery at Ballsh. Such viscosity reduction is not necessary for international export by tanker ship and hence the assay sample was taken upstream of Tank No. 43, In Tank

211

Tank No. 41 has sample points at 5 different levels, corresponding to tank contents of nominally 20%, 30%, 40%, 50%, 65%, 80% and 90% full. The 20% sample point is near the bottom of the tank and the 90% sample point is near the top.

During the last few days of sample period production, samples were taken from various levels and

BS&W was measured using AAP field laboratory facilities. Initial samples from various levels had BS&W up to 12%. 34 m3 was then transferred out of the bottom of the tank and BS&W was reduced to between 2% (high sample point) and 7% (low sample point). After a 9 hour soak period, these figures reduced to 2% to 3%. After a further 6 hour soak period, the figures were generally less than 2%.

The actual assay samples were then taken from the 80% level (251 m contents) in the tank, and BS&W was measured in the field as 1.9% (being 0.5% sand and 1.4 % water).

The total oil volume taken for sampling was:

- * 3 x 200 litre plastic drums (for buyer samples)
- * 5 x 10 litre brand new metal containers (for assay)
- * 1 x 1 litre sample for locat testing by AAP and che labs in Fier and Kucova

we were advised that 5 litres was the maximum container size acceptable for air freight. Also, the maximum amount permitted on a single flight was 5 x 5 litres. Thus, the sample was alr,,freighted In 2 lots of 5 x 5 litre samples.

(The metal containers are purpose designed for air and sea freight and have actual volumes more like 1 L5 litres and 5.75 litres. Nominal capacities are 10 litres and 5 litres.) The whole crude oil sample was also analysed locally and results were as follows:

Density (D15/15C) = 0.996 gm/cc (from AAP and Kucova)

BS&W = 1.9% (from AAP and Kucova)

Water cut = 1.4% (from AAP and Kucova)

Sand cut = 0.5% (from AAP and Kucova)

Viscosity at 30 °C = 5208 CP (from Fier)

Viscosity at 40 °C = 2361 CP (from Fier)

Viscosity at 50 °C = 1157 CP (from Fier) 9

WHOLE CRUDE

Density	150C	Intl	1.0001
API Gravity	60/60°F	60/60QF	9.9
Total Sulphur			5.82
Mercaptan Sulphur			627
Hydrogen Sulfide		m Wt	
Total Nitrogen		m Wt	1578
Reid Vapor Pressure		si	UIS

Pour Point		

Laboratory Report 03-004386-0-ABDN Page of

Kinematic Viscosi 400C	cSt	4010
Kinematic Viscosi 100oc	cSt	
D namic Viscosi 40°C	centi oise	3951
D namic Viscosi 100oc	centi oise	1086
Or anic Chloride	mWt	0.4
Conradson Carbon		16.0
Total Acid No	m KOHI	0.56
Wax Content		
Nickel	mWt	60
Vanadium	mWt	311
As hlatenes		14.8
Ash Content	°	
Salt Content	m Il	
Water Content	O/ovol	0.55
BS&W	O/ovol	085
Flash Point	°c	33
Methane		<0.01
Ethane		<.0. 01
Pro ane		<0.01
Isobutane	%Wt	<0.01
n-Butane	%Wt	<0.01
Neo entane	%Wt	<0.01
Iso entane		0.05

n•Pentane		0.05
C clo entane		0.01
Hexanes+		99.89

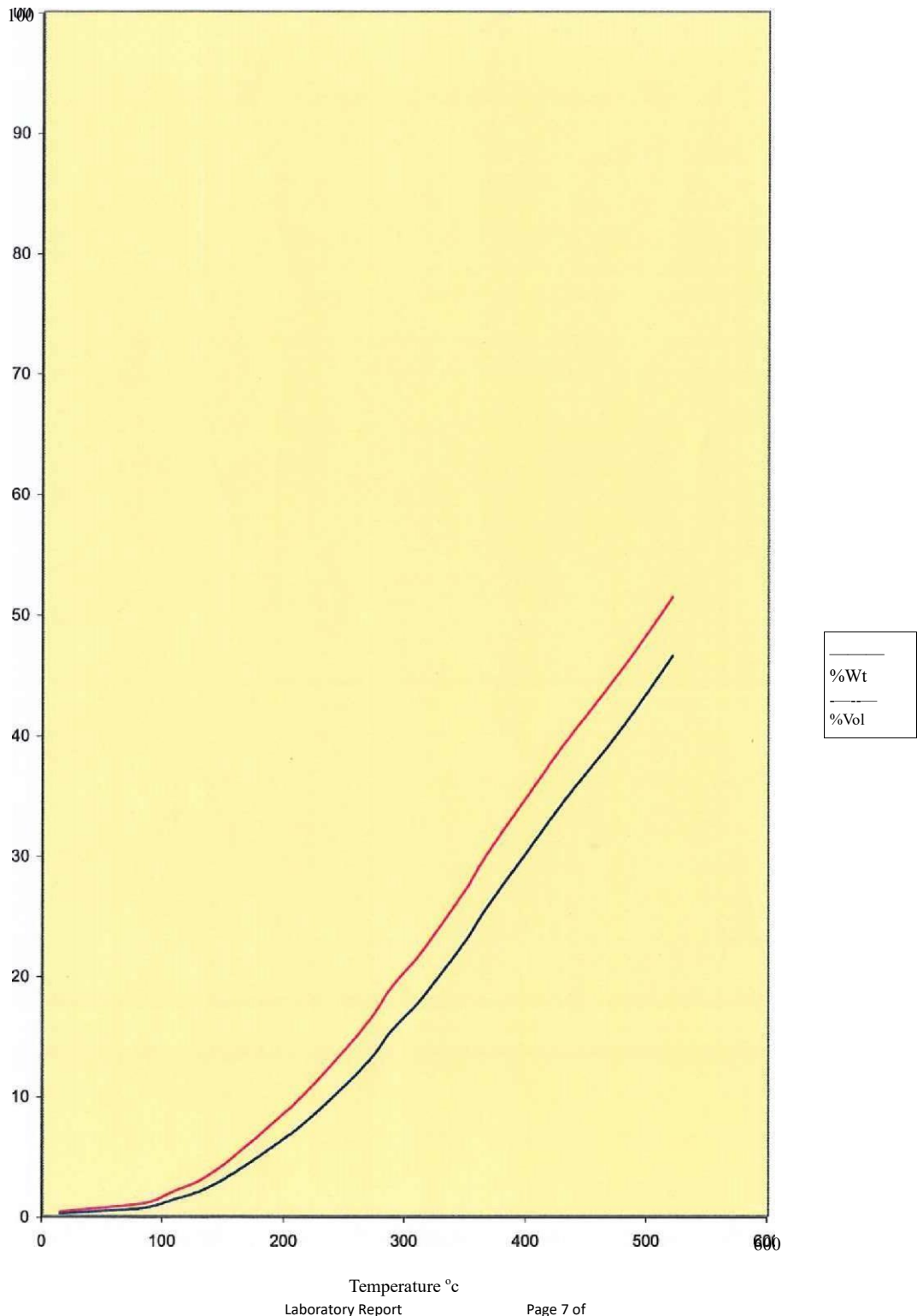
TRUE BOILING POINT DISTILLATION

Tem De F	Tem De c	Cum	Cum %Vol	Densi 150C	API Gravi
				0,5650	
				0,6790	7618
194	90.0	0,75	1.17	0.7098	67.7
				o. 7339	61.2
				o. 7524	56.5
				o. 7730	
329	165.0	3,99	5.49	0.7862	48.4
374	190.0	5.71	7.67	0.8108	42.9
410	210.0	7.20	9.49	0.8310	38.7
446	230.0	8,91		0,8432	36.2
	250.0		13.80	0,8643	32.1
518	270.0			0,8802	292
	290.0			0,8932	26.8
590	310.0		21.47	0.9091	24.1
	325.0	19,53	23.56	0.9151	23.1
	350.0	22.87		0.9325	20.2
698	370.0	25.99	30.43	0.9461	
		33.60		0.9591	16.0
	450,0	36.78	41.59	0.9677	14.7
	475.0	40.00	44.87	0.9767	13.3
932	500.0	43.42	48.30	0.9885	11.6
970	521.0	46.49	51.39	0.9980	10.2
970 + Res	521 + Res	100.00	100.00		-2.9

Laboratory Report

jurisdiction

Any holder advised instructions, any. The
responsiblilty transaction
documents. Any alteration. the law. "
True Boiling Point Curve Patos-
Marinza



NAPHTHAS

Bolln Ran e	oc	cs • 70	70 -165	- 190
-------------	----	---------	---------	-------

Yield		0.50 0.33		2.18 1.73
	%Wt		3.46	
Densi		0.6790	0.7621	0.8108
API Gravi 601604F		76.77	54.07	42.93
Toca\$ Sul hur		0.13	0.48	1.28
Merca tan Sul hur	mWt	326	324	64
Total NHro en	mWt			
RefdVa our Pressura	sl	95		
Paraffins		78.39	42.95	32.66
Na hthenes		20.09	43.90	39.18
Aromaticcs	a, 'owt	1.52		24.17
Boilin >2CO'C	%Wt	<0.01		3.99
Research Octane No		IIS	IIS	US
esearch Octane Na 0,15 li TEL		IIS	us	IIS
Motor Octane No		VS	FIS	IIS
Motor Octane No 0.15 li TEL		us	fis	IIS
Pour Point				
CFPP				
Cloud Point	oc			
Freeze Point				
Catane Index				28.3
ASTM Colour				LO.5
Kinemauc Viscosi	cSt est			0.9893
Kinemauc Viscosi logec				0.5587
D namEc VI\$cosit	cent' Oise			0.7843
O namic Viscosi looac	centi aise			0.4184
Smoke Point	mm			22
Co er Strl Corrosion			4b	46
3hrs loo °c				
Or anlc ChEoride	mWt	4.4	1.1	1.4

Na thalenes	%Vol			0.04
-------------	------	--	--	------

Flash Point				56
Point	oc oc	26,6	28.6	132.0
5% Recove		27.8	76.1	
10% Recove		35.5	90.3	159,3
20% Recovery	°C	55.4	1028	165.3
			115.8	
Recove Recove		58.8		170.0
	°C	62.7	123.0	173.8
Recove	oc			
		64.5	133.8	
Recove			140.1	
		39.7		180.5
Racove				
		75.4	146.0	183.7
Recove		83.7	154.3	
Reeove	oc	90.1		
95% Recovery	oc	94.1		
Final eolRn Point	oc		179.0	203.2

KEROSENES/GAS OILS

Bollin Range		190 -230	230 - 325	325 • 370
Yield	vol%	3.89	12.00	6.87
		3.20	10.62	6.46
Density 150C	lml	0.8375	0.8902	0.9427
API Gravity		37.37	27.38	18.64
Sulfur Content		1.50	3.04	4.38
Mercaptan Sulfur	mWt	44	70	141
Total Nitrogen	mWt		68	596
Basic Nitrogen	mWt		30	140
Pour Point				
Cetane Fpp	°C			2
Cloud Point	°C			
Freeze Point	°C			
Cetane Index		31.1	35.5	34.6
UOP'K'				
ASTM Colour		LO.5	1.0.5	
Kinematic Viscosity 400G		1.406	3.391	12.69
Kinematic Viscosity 100°C	cSt			2.702
Dynamic Viscosity 400C	centipoise		2.961	
Dynamic Viscosity 100°C	centipoise	0.5534		2.392
Smoke Point	mm	18		
Corrosion		4a	3b	
3Hrs 100°C				
Aniline Point	°C	42.6	43.8	44.4
Aromatics	%Vol	28.3		
Organic Chloride	mWt	1.3	1.5	1.3
Conradson Carbon				0.03
Total Acid No	m KOW	0.56	1.03	1.08
Ref Index				1.50135

jurisdiction

Any holder advised instructions, any. The responsibility transaction documents. Any alteration. the law. "

Na *halenes	%Vol	1.62		
Wax Content				< 1.0
Flash Point	-C	69	109	
initial Boilin Point	-C			294.0
5% Recove	-C	184.4	230.1	
10% Recove	•C	190.2	237.0	322.5
20% Recove	•C	197.0	250.3	330.5
30% Recove	•C	202.3	259.5	336.5
40% Recove	•C		2697	342.0
50% Recove			279.3	347.0
60% Recove		214.9	2886	352.0
70% Recove		219.4	298.5	357.0
80% Recove		224.4	308.2	362.5
90% Recove	•C	230.2	318.3	369.0
95% Recove		233.5	324.2	
Final Boilin Point	•C	245,6	335.0	386.5

Laboratory Report

VACUUM GAS OILS

Boilin Ran e	•C	370 -521
		20.96
		20.50
Densi	lml	0.9759
API Gravi	60160*	13.43
Sul hur Content		5.00
Total Nitro en	mWt	1286
Basic Nitro en	mWt	433

Pour Point		-3
------------	--	----

UOP%		
Kinematic Viscosity @ 40°C	cSt	
Kinematic Viscosity @ 100°C	cSt	
Density @ 40°C	centi Ounce	187.6
Dynamic Viscosity @ 100°C	centi poise	10.80
Aniline Point		53.4
Conradson Carbon Residue	%Wt	1.12
Total Acid No	mg KOH/g	0.22
Refractive Index @ 20°C		1.62234
Wax Content	%Wt	<1.0
	mgWt	<0.1
Vanadium	mgWt	0.2
Sodium	mgWt	0.1
Initial Boiling Point		352.0
5% Recovery	°C	372.0
10% Recovery		381.5
20% Recovery		397.5
30% Recovery	°C	412.0
40% Recovery	°C	426.0
50% Recovery		439.5
60% Recovery	°C	454.0
Recovery		469.0
80% Recovery	°C	485.0
90% Recovery	°C	505.0
Recovery		
Final Boiling Point		554.0

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Laboratory Repoli 03-004386.O*ABDN

RESIDUE

Boilin Ran e	oc		
--------------	----	--	--

Yield	vol%	69.57	48.61
Densi 150C	lml	1.0640	1.1000
API Gravi 60160CF		1.44	-2.91
Sul hur Content		6.92	7,76
Total Nitro en	mWt	2190	2500
Basic Nitro en	mWt	1350	1599
Pour Point	oc	51	129
UOP'K'			
Kinematic Viscosi 100°C	cSt	2462	
Kinematic Viscosi 1350C	cSt	798.6	
Kinematic Viscosi 1509C	cSt		5283
D namic Viscosi 1000C	centi Oise	2484	
D namic Viscosi 135°C	centi Oise	787.4	
D namic Viscosi 150'C	centi Oise		5400
Conradson Carbon Residue	%Wt	23.5	32.5
Total Acid No	m KOHI	0.13	0.22
Wax Content			<1.0
Nickel	mWt	86.9	138
Vanadium	mWt	436	608
Sodium	mWt	80.2	84
Softnin Point	oc	41.4	98
Pentration 25 ⁹ C		68	

As haltenes		192	262
Ash Content	O/awt	0.227	0,573
Initial Boilin Point		365.0	476.0
5% Recove	OC	398.0	521 .o
10% Recove		426.0	539.5
Recove	oc	479.5	569.5

30 °/0 Recove	oc	528.5	598,0
40 °/0 Recove	oc	568.0	628.0
50% Recove	oc	608.5	658,5
60°/0 Recove	oc	650.5	695.5
70% Recove	oc		
Final Boilin Point	oc		
Recove		723	64.6

TEST METHODS

Test

Ash Content Asphaltenes

ASTM Distillation

ASTMD2887

Basic Nitrogen by Direct Titration

CBA 73

BS&W

ASTMD4007

C1 C5 Determination

IP 344

Cetane Index

ASTM 02500

I P 380

Cloud Point

ASTM D189 ASTM

Conradson Carbon Residue

DI 30

Copper Strip Corrosion

ASTM D4052/ASTMD287 *

Density/API Gravity Flash

I P 365

Point

ASTM 02386

Freezing Point

(JOP 163

H2S and RSH in Distillates

ASTM 01319

Hydrocarbon Types by FIA

ASTM 0445

Kinematic Viscosity

CBA21

Metals

ASTMD2700

Motor Octane Number

ASTM 01840

Naphthalenes

CBA4

Paraffin Wax Content

Penetration PNA

IP382

Pour Point

ASTM D97

Pour Point on Crude

ASTMD5853

Refractive Index

ASTMD1218

Reid Vapour Pressure

ASTM D323

IP69

Research Octane Number	ASTMD2699	
Satt Content	ASTM D3230	tP265
Smoke Point		
Softning Point		
Sulphur	ASTMD4294 *	
Totat Acid Number	ASTM D664	
Total Nitrogen	ASTM D4629 *	
True Boiling Point Distillation	ASTM D2892/ASTM D5236	
I-JOP K Factor Water in Crude Oil	Calculation	

APPENDIX C - POTENTIAL BUYERS

KASTRATI

Adresa: L 14, "Ura e Dajlanit", ShkozetyDures Tel : +355 52 65 170 / Fax: +355 52 65 166

Subject: Letter of Interest

To:

"OIL PALMIR" JSC

Dear Sir!

"KASTRATI", a joint stock company registered under the laws of Republic of Albania, with its legal seat at: Lagjia 14, Ura e Dajlanit⁹ Dures, Albania, with registered fiscal no. K 21711502 V, duly represented by its Administrator Mr. Gani Kastrati, with its main activity on the wholesale of the hydrocarbons and their by-products is interested to cooperate and to have a partnership with "OIL PALMIR" JSC, an Albanian company with its legal seat at: Lagjia 29 Marsi, Patos, Fier, Albania, with registered fiscal no. L 23401403 P, duly represented by its Administrator Mr. Perparim Gropa.

"KASTRATI" JSC is willing to be supplied with standard oil products such as Euro — Diesel and Unleaded Gasoline as soon as "OIL PALMIR" JSC will terminate the construction of its crude oil refinery and start the trading of the hydrocarbons.

Through the present letter of interest "KASTRATI" JSC shows its readiness to conclude at that time a proper and detailed agreement with "OIL PALMIR"⁹ JSC specifying the terms and the conditions of the fuel supply.

Best Regards,

Mr. Gani KASTRATI

Administrator



Shoqëria 'iBo/v-Oi/' Sh.a.

Fier, Shqipëri

NUIS:

1<32528408H Tel:

+355 67 20 74 117

www.bolv-oi/.a/

Letter of Interest

To: "OIL PALMIR" JSC

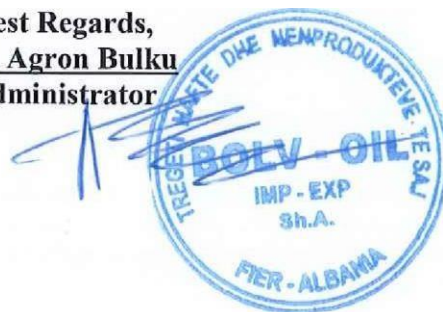
Dear Sir!

"BOLV OIL" JSC, a joint stock company registered under the laws of Republic of Albania, with its legal seat at: Rruga "Fier Patos Km - 6", Fier, Albania, with registered fiscal no. K32528408H, duly represented by its Administrator Mr. Behar CUKO, with its main activity on the wholesale of the hydrocarbons and their by-products is interested to cooperate and to have a partnership with "OIL PALMIR" JSC, an Albanian company with its legal seat at: Lagjia 29 Marsi, Patos, Fier, Albania, with registered fiscal no. L 23401403 P, duly represented by its Administrator Mr. Perparim Gropa.

"BOLV OIL" JSC is willing to be supplied with standard oil products such as Euro - Diesel and Unleaded Gasoline as soon as "OIL PALMIR" JSC will terminate the construction of its crude oil refinery and start the trading of the hydrocarbons.

Through the present letter of interest "BOLV OIL" JSC shows its readiness to conclude at that time a proper and detailed agreement with "OIL PALMIR" JSC specifying the terms and the conditions of the fuel supply.

**Best Regards,
Mr. Agron Bulku
Administrator**



Contact Data:

Mob.: (+355) 67 20 54 441;

E-mail: a.bulku@bolv-oil.al



*Adresë kontakti: "Pika Karburantit "Bolv-Oil", prapa Casa Italia, pranë Godinës së Top-Channel,
Mëzëz, Kashari Tiranë, Shqipëri*

Contact Data:

Mob.: (+355) 67 20 54 441;

E-mail: a.bulku@bolv-oil.al

(Albania)

TRANSOILGROUP AG

Schönbielpark 10, Ch 9016 St. Gallen, Switzerland

Transmlgroup Sh.A
NIPT L117250041
Rr. "Ismail Qemali"
Pallati "Fratari Construction"
AP. 8/A, Tirane
Tel. 00355 4 2274
814 Fax. 00355 4
2274 816

Dear Sir!

"TRANSOIL GROUP" JSC, a joint stock company registered under the laws of Republic of Albania, with its legal seat at: Road "Ismail Qemali", Tirane, Albania, with registered fiscal no. L1 1725004 1, duly represented by its Director of Operations at Visoka Oilfield Mr. Edmond BEJTAJ, with its main activity on the wholesale of the hydrocarbons and their by-products is interested to cooperate and to have a partnership with "OIL PALMIR" JSC, an Albanian company with its legal seat at: Lagjia 29 Marsi, Patos, Fier, Albania, with registered fiscal no. L 23401403 P, duly represented by its Administrator Mr. Perparim Gropa.

"TRANSOIL GROUP " JSC is interested to the sale of products crude oil and gases as soon as "OIL PALMIR" JSC will terminate the construction of its crude oil refinery and start the trading of the hydrocarbons.

Through the present letter of interest "TRANSOIL GROUP " JSC shows its readiness to conclude at that time a proper and detailed agreement with "OIL PALMIR" JSC specifying the terms and the conditions of the fuel supply.

Best Regards,

Mr. Edmond BEJTAJ

Director of Operations at Visoka Oilfield



FIN PEK PETROLEUM Shea

Adress: Fier-Patos Ian 6

E-mail: finpek@yahoo.com

Tel: 0682085196

INTEREST LETTER

THE COMPANY FinPek Petroleum Sh.a with activity in field of Hydro carbon for emission of crude oil in area Finiq-Krane & Pekisht,,Murriz is interested that with construction of Refinery by The Company " OIL PALMIR " s.a (With authorization of Energetic Ministry of year 2014) with construction of Refinery after 2 years , to supply with crude oil the Company OIL PALMIR according the prices on International Market.In profit and in our interest.

THE ADMINISTRATOR



Adresa: '1Lagja

Xhevdet Nepravishta" Lughnje Web:

www.oaet.eu E-mail: aeotsha@yahoo.com Cel:

0694010514

Subject: Letter of Interest

Lushnje

To: "OIL PALMIR" JSC

Dear Sir!

"AEOT" JSC, a joint stock company registered under the laws of Republic of Albania. with its legal seat at: Lagja "Xhevdet Nepravishta", Lushnje, Albania, with registered fiscal no. L32604402E, duly represented by its Administrator Mr. Ardian Kulla, with its main activity on the wholesale of the hydrocarbons and their by-products is interested to cooperate and to have a partnership with "OIL PALMIR" JSC, an Albanian company with its legal seat at: Lagja 29 Marsi, Patos, Fier, Albania, with registered fiscal no. L 23401403 P, duly represented by its Administrator Mr. Perparim Gropa.

"AEOT" JSC is willing to be supplied with standard oil products such as Euro Diesel and Unleaded Gasoline as soon as "OIL PALMIR" JSC will terminate the construction of its crude oil refinery and start the trading of the hydrocarbons.

Through the present letter of interest "AEOT" JSC shows Its readiness to conclude at that time a proper and detailed agreement with "OIL PALMIR" JSC specifying terms and the conditions of the fuel supply.

Best Regards,
Mr. Ardian KULLA
Administrator



Subject: Letter of Interest

To: "OIL PALMIR" JSC

Dear Sir!

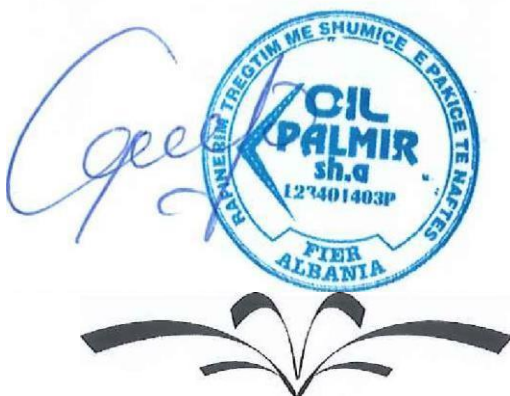
"PHOENIX PETROEUM " Jsc, a joint stock company registered under the laws of Republic of Albania, with its legal seat at: Road "Elbasanit", Tirane, Albania, with registered fiscal no. K92927401K, duly represented by its Administrator Mr. Naim KASA, with its main activity on the wholesale of the hydrocarbons and their by-products is interested to cooperate and to have a partnership with "OIL PALMIR" JSC, an Albanian company with its legal seat at: Lagjia 29 Marsi, Patos, Fier, Albania, with registered fiscal no. L 23401403 P, duly represented by its Administrator Mr. Perparim Gropa.

"PHOENIX PETROLEUM" JSC is interested to the sale of products crude oil and gases as soon as "OIL PALMIR" JSC will terminate the construction of its crude oil refinery and start the trading of the hydrocarbons.

Through the present letter of interest "PHOENIX PETROLEUM" JSC shows its readiness to conclude at that time a proper and detailed agreement with "OIL PALMIR" JSC specifying the terms and the conditions of the fuel supply.

Best Regards

Best Regards
Mr. Naim KASA
Administrator



AlbDRAIlInq

Subject: Letter of Interest

Patos

To: "OIL PALMIR" JSC

Dear Sir!

"ALB DRILLING" JSC, a joint stock company registered under the laws of Republic of Albania, with its legal seat at: Rruga "Fier Patos Km 6", Fier, Albania, with registered fiscal no. L 43512401 N, duly represented by its Administrator Mr. Agron SHEHU, with its main activity on the wholesale of the hydrocarbons and their by-products is interested to cooperate and to have a partnership with "OIL PALMIR" JSC, an Albanian company with its legal seat at: Lagjia 29 Marsi, Patos, Fier, Albania, with registered fiscal no. L 23401403 P, duly represented by its Administrator Mr. Perparim Gropa.

"ALB DRILLING" JSC is interested to the sale of products crude oil and gases as soon as "OIL PALMIR" JSC will terminate the construction of its crude oil refinery and start the trading of the hydrocarbons.

Through the present letter of interest "ALB DRILLING" JSC shows its readiness to conclude at that time a proper and detailed agreement with "OIL PALMIR" JSC specifying the terms and the conditions of the fuel supply.

Best Regards,
Mr. Agron SHEHU
Administrator
a.shehu albrillin .al cell:
069 60 60 128



PORTO ROMANO OIL SH.A.,

Adresa: Zona energjetike, Porto Romano, Durrës, Shqipëri (Albania)



Tel.' +355 67 20 19523
NUIIS: 1<613305011
Magazina e liré doganore ML-05 www.bo/v-oil.a/

Letter of Interest

To: "OIL PALMIR" JSC

Dear Sir!

"PORTO ROMANO" JSC, a joint stock company registered under the laws of Republic of Albania, with its legal seat at: Rruga "Porto Romano", Durrës, Albania, with registered fiscal no. K613305011, duly represented by its Administrator Mr. Robert Stoja, with its main activity on the wholesale of the hydrocarbons and their by-products is interested to cooperate and to have a partnership with "OIL PALMIR" JSC, an Albanian company with its legal seat at: Lagjia 29 Marsi, Patos, Fier Albania, with registered fiscal no. L 23401403 P, duly represented by its Administrator Mr. Perparim Gropa,

"PORTO ROMANO" JSC is willing to be supplied with standard oil products such as Euro Diesel and Unleaded Gasoline as soon as "OIL PALMIR" JSC will terminate the construction of its crude oil refinery and start the trading of the hydrocarbons.

Through the present letter of interest "PORTO ROMANO" JSC shows its readiness to conclude at that time a proper and detailed agreement with "OIL PALMIR" JSC specifying the terms and the conditions of the fuel supply.

Best Regards,
Mr. Robert STOJA
Administrator

Contact Data:

Mob.: (+355) 67 201 9523;
E-mail: info@pro.al



AGREEMENT

between:

STK Volga Ltd, company registration number: 20118614739 registered in Bulgaria,
Plovdiy, Blvd.6-th September 125, represented by Mrs. Irena Vasileva

and

1 . Oil Palmir SHAY a joint stock company registered in Albania, with NIJIS/NIPT
L,23401403P, seated in Albanias Patos, Lagjja 29 Marsi, Kilometri i 6 Fier-Patos,
represented by Mr. Perparim Gropa, in the quality of the legal representative of the
company, hereinafter referred to as the Company,

Referred jointly as the Parties.
Considering that,

o The Company has already obtained a government license to build and operate an oil
refinery in Albania which shall be constructed in Portéz, Patos-Marinéz area, Albania.

The parties agree and enter into the following agreement:

1. The object of the agreement will be cooperation in the field of hydrocarbons, concretely
supplying with crude oil.



21 The company "STK Volga" will supply Oil Palmir SHA with crude oil according to the processing capacity of the refinery after completion of construction of the refinery.

3, After completion of construction of the refinery this collaboration between parties will be materialized with the contract signed by them with terms not less than 10 years, The contract will be specified: the quantity of crude oil with which will be supplied Oil Palmir SHA ; the price; the transport ; the rights and obligations of the parties and other details necessary.

4. No modification of the terms of this Agreement shall be valid unless made in writing and signed by authorized representatives of the parties,

This Agreement entered on day of signature by the parties.

COMPANY

Oil Palmir SHA

represented by the administrator

Përparim Gropa



PANY

Represented by the Mr.

Përparim Gropa Date:

COMPANY

STK Volga

Irena Vasileva

Date: 09.05.2014



APPENDIX D - RENEWAL OF THE REFINERY LICENSE

THE GOVERNMENT LAW No. 8450, dated 24.2.1999

DECISION

NO. 19, DATED 14.1.2015

ON THE PROCEDURES AND CONDITIONS FOR THE GRANTING, TRANSFER AND RENEWAL OF THE REFINERY CONCESSION LICENSE FOR CARRYING OUT THE ACTIVITY OF PROCESSING CRUDE OIL FOR THE PRODUCTION OF ITS BYPRODUCTS

In accordance with Article 100 of the Constitution and Articles 12, point 2, and 18, point 3, of Law No. 8450, dated 24.2.1999, “On the processing, transportation and marketing of oil, gas and their by-products”, as amended, upon the proposal of the Minister of Energy and Industry, the Council of Ministers

DETERMINED:

I. GENERAL PROVISIONS

1. Any legal entity, established under the provisions of Law No. 9901, dated 14.4.2008, “Ontraders and commercial companies”, as amended, and organized in the form of a joint stock company, may apply for a Refinery Concession License to carry out the activity of processing crude oil for the production of its by-products, in accordance with the rules set out in this decision, based on the principles of non-discrimination, equal treatment and transparency.
2. The Refinery Concession License to carry out the activity of processing crude oil for the production of its by-products is obtained by interested legal entities, after providing them with the prior approval as provided for in Chapter II and after fulfilling the conditions set out in Chapter III of this decision.

II. CONDITIONS AND PROCEDURES FOR THE PRELIMINARY APPROVAL OF EQUIPMENT

1. Legal entities that request to be provided with a Refinery Concession License to carry out the activity of processing crude oil for the production of its by-products, before the start of the construction and commissioning of the refineries, submit to the ministry responsible for hydrocarbons a request to be provided with a preliminary approval in order to continue the procedure, accompanied by the following documents:
 - 1.1 Extract from the commercial register from the National Registration Center, where it is certified that the legal entity is organized in the form of a joint-stock company and where it has defined in its scope of activity the processing of crude oil and its by-products and that the status of the legal entity is active.
 - 1.2 The scheme and technological project for each plant, which will be applied for the construction of the refinery and the infrastructure facilities, which ensure its normal functioning, including the fire protection project, the technological waste treatment project, the material balance and the forecast of financial indicators.
 - 1.3 The scheme of supply of raw materials and auxiliary materials.
 - 1.4 The preliminary feasibility study for the activity to be carried out by the legal entity.
 - 1.5 The environmental declaration at the end of the in-depth environmental impact assessment procedure, issued by the minister responsible for the environment, according to the legislation in force.

- 1.6 The master plan of the site where the refinery is planned to be built, as well as the presentation of relevant documentation proving the applicant's relationship with the land where the refinery is planned to be built (ownership certificate, purchase contract or lease contract, etc., for a period not less than the validity of the refinery concession license).**
 - 1.7 The document certifying that the use of the land where the refinery will be built is foreseen for the construction of facilities of this nature in one of the territorial planning instruments according to the provisions of Law No. 107/2014, dated 31.7.2014, "On territorial planning and development".**
 - 1.8 Documentation certifying experience in the field of construction and commissioning of refineries.**
 - 1.9 Documents in the form of a letter of interest, preliminary credit agreement or any other document, confirming the financial support of the project from financial institutions or domestic or foreign banks, clearly stating the monetary values for financing and the financing structure (applicant's own financing, bank loans, donations or other financing) for the construction of the refinery.**
 - 1.10 Declaration on the value of the license signing bonus offered by the legal entity in the case of being granted a Refinery Concession License. The value of the bonus offered in any case must not be less than 1,000,000 (one million) lek. In this case, the declaration must be accompanied by a bank financial guarantee for the full value of the bonus, based on which the payment of this bonus is guaranteed immediately upon signing the Refinery Concession License.**
 - 1.11 The value of the annual training bonus offered by the legal entity in the case of being granted a Refinery Concession License.**
 - 1.12 Document certifying that the legal entity has not been convicted by a final decision related to the company's activity, issued by the court.**
 - 1.13 Document certifying that the representative of the legal entity is not under criminal prosecution, issued by the prosecutor's office.**
 - 1.14 Document certifying that the legal entity has fulfilled its fiscal obligations, issued by the tax administration.**
 - 1. 15 Document certifying that the legal entity has paid all social security obligations, issued by the tax administration.**
 - 1.16 Document certifying the payment of electricity for each premises where the applicant company carries out its activity.**
- The certifying documents must be drawn up in Albanian, original or notarized photocopies. For documents translated into Albanian, the certification of the translator's signature is made by a notary.**
- 2. For the assessment of the requests and accompanying documentation submitted by legal entities to be provided with prior approval for the continuation of the procedure for the provision of a Refinery Concession License, an assessment committee is established by order of the responsible minister, who also determines its mode of operation. 2.1 The assessment committee must be composed of representatives from:**
 - the ministry responsible for the hydrocarbon sector, 3 (three) members;**
 - the ministry responsible for urban development and tourism, 1 (one) member;**
 - the ministry responsible for the economy, 1 (one) member; - the ministry responsible for the environment, 1 (one) member; - the ministry responsible for local government, 1 (one) member.**
 - 2.2 The application evaluation committee shall evaluate the applications and documentation submitted by the legal entity, as defined in point 1, chapter II, of this decision.**

In the event that for the same land area there is more than one legal entity that meets the conditions for granting prior approval to continue the procedure for obtaining a Refinery Concession License, as a selection criterion, the committee shall use the value of the bonuses offered by each legal entity at the disposal of the state budget and the technological project that will be applied for the construction of the refinery. In this case, based on the criteria of the value of the bonuses offered and the technological project, the evaluation commission reviews all applications and proposes to the minister responsible for hydrocarbons to grant preliminary approval to the applicant who proposes the best solution.

3. The application evaluation commission meets within 30 (thirty) days from the date of submission of the application, verifies the relevant application documentation and acts as follows.

a) When, after verification, it results that the documentation submitted by the legal entity is irregular, the commission accepts the application and, within 15 (fifteen) days from the date of the meeting, submits to the minister responsible for hydrocarbons the proposal for preliminary approval for further continuation of the procedure for completing the technical and economic documentation for the facility in the requested area and surface and for carrying out the relevant practices until obtaining the Refinery Concession License;

b) When the review of the documentation and the verifications carried out in other institutions and/or in the field show that the required conditions are not met, the commission shall draft a report and notify the applicant of the missing documentation and its right to complete the documentation and the relevant conditions no later than 30 (thirty) calendar days from the date of the initial notification;

The applicant has the right to resubmit the application with the completed documentation within 30 (thirty) calendar days from the date of notification. The commission shall meet and make a decision within 10 (ten) calendar days from the date of submission of the completed documentation or within 10 (ten) calendar days from the date of expiry of the submission deadline if the applicant has not completed the documentation.

c) When, after the final verification, it results that the submitted documentation does not meet the conditions set out in point 1, of Chapter II, of this decision, the commission rejects the request and, within 10 (ten) days from the date of the meeting, returns the relevant documentation to the legal entity, where the decision taken is argued. The legal entity has the right to reapply after completing and correcting the documentation.

c) When the legal entity does not agree with the decision of the commission, it has the right to appeal within 10 (ten) days from the date of the decision, to the minister responsible for hydrocarbons.

4. The preliminary approval must contain at least the following data:

a) The name of the legal entity submitting the request and the NIPT;

b) The right to prepare complete documentation in the relevant area, in accordance with the requirements of the legislation in force for obtaining the Refinery Concession License from the Council of Ministers;

c) The time limit for the validity of the approval for the continuation of the procedure, within which the preparation of the necessary documentation for obtaining the Refinery Concession License must be completed until its submission to the ministry responsible for hydrocarbons for further processing.

In any case, this period cannot exceed two years.

III. PROCEDURES FOR OBTAINING A REFINERY CONCESSION LICENSE

1. Person legal entity, provided with prior approval for the continuation of the procedure, must submit to the ministry responsible for hydrocarbons, within the deadline specified in letter “c”, point 4, chapter II, of this decision, the documentation for obtaining the Refinery Concession License. This documentation must contain:

- 1.1 an extract from the commercial register from the National Registration Center of the legal entity, where it is determined in the scope of its activity the processing of crude oil and its by-products and that the status of the legal entity is active;
 - 1.2 the environmental permit of the activity, issued by the responsible body;
 - 1.3 the development permit, according to the provisions of law no. 107/2014, dated 31.7.2014, "On territorial planning and development";
 - 1.4 detailed technological project for the construction of the refinery and infrastructure facilities, which ensure the normal functioning of the refinery, including the fire protection project, the technological waste treatment project, the material balance and financial indicators. The technological project must also be approved by the responsible State Inspectorate;
 - 1.5 feasibility study for the activity to be carried out by the legal entity;
 - 1.6 technological card with work parameters and final products obtained in accordance with the standards in force, approved by the responsible State Inspectorate;
 - 1.7 employment contract of the technical manager who will follow the implementation of the refinery project and its commissioning;
 - 1.8 the master plan of the site where the refinery is planned to be built, as well as the relevant documentation proving the applicant's relationship with the land where the refinery is planned to be built (ownership certificate, purchase contract or lease contract, etc. for a period not less than the validity of the refinery concession license);
 - 1.9 a document certifying that the legal entity has not been convicted by a final decision related to professional activity, issued by a court;
 - 1.10 a document certifying that the representative of the legal entity is not under criminal prosecution, issued by the prosecutor's office;
 - 1.11 documentation in the form of a letter of interest, preliminary credit agreement or any other document, certifying the financial support of the project from domestic or foreign financial institutions or banks, clearly stating the monetary values for financing and the financing structure (applicant's own financing, bank loans, donations or other financing) to cover the construction of the refinery.
2. The Refinery Concession License shall be prepared by the structure responsible for hydrocarbons in the ministry responsible for hydrocarbons in cooperation with the applicant legal entity or its legal representative.
 3. The Refinery Concession License, together with all documents prepared pursuant to this decision, including a copy of the preliminary approval for the continuation of the procedure, shall be submitted for approval to the Council of Ministers.
 4. The Refinery Concession License shall contain at least the following data:
 - a) Name and headquarters of the legal entity; b) Coordinates and location of the refinery;
 - c) Number and date of the decision of the National Territorial Council for the approval of the development permit;
 - c) Type of trading license and its term, if the legal entity is equipped with this license;
 - d) The validity period of the concession license, as well as the right to renew this license through the submission of a request by the legal entity according to the procedures set out in Chapter V of this decision; d) The deadline for completing the construction of the refinery, the deadline for putting it into use, as well as the cases when an extension of the construction or putting it into use period will be allowed;

e) The right of state bodies and institutions, charged by law, to control the implementation of the project according to the conditions and deadline set out in the project;

ë) The right of the Council of Ministers to revoke this license when the controls exercised by state bodies and institutions, charged by law, establish a failure to meet the requirements of the Refinery Concession License, in the implementation of technical parameters, in the deadline for the implementation of the project and in environmental standards; f) The capacity and category of products that the refinery will produce;

g) Financial obligations that the legal entity has towards the state in relation to the concession license; gj) The obligation to implement the requirements of Articles 9 and 12 of Law No. 8450, dated 24.2.1999, for maintaining the safety reserve, changes in the scheme and technological card of the refinery's operation, as well as for the brand and quality of oil by-products produced by the refinery;

h) The data that the legal entity must submit to the ministry responsible for hydrocarbons, within the deadlines in accordance with the order of the minister.

The Refinery Concession License, in accordance with the legal provisions in force, may also include definitions other or mutual obligations.

5. The Refinery Concession License is drawn up in three copies, of which one copy is kept in the ministry responsible for hydrocarbons and one copy is officially forwarded to the legal entity to which the concession license is granted and to the Council of Ministers.

6. The granting of the Refinery Concession License for the construction of a refinery for the processing of crude oil and its operation is made against the payment of a fee of 30,000,000 (thirty million) lek by the legal entity, the amount of which is paid entirely into the state budget.

7. The Council of Ministers has the right to revoke the concession license when, during the controls carried out by state bodies and institutions, charged by law, it ascertains a violation or non-compliance with the requirements of the Refinery Concession License, nonimplementation of the technical parameters of the project and non-compliance with the project implementation deadline, environmental standards and other obligations provided for in the license that are determined by the legislation in force.

8. The legal entity equipped with a concession license, in accordance with the terms and conditions set out in this license, submits the application and relevant documentation for obtaining a construction permit for the facility in accordance with the procedures set out in Law No. 107/2014, dated 31.7.2014, "On territorial planning and development". Upon completion of the construction of the refinery, the legal entity submits the application and relevant documentation for obtaining a certificate of use of the facility in accordance with Law No. 107/2014, dated 31.7.2014, "On territorial planning and development".

IV. PROCEDURES FOR TRANSFER OF REFINERY CONCESSION LICENSE

1. The transfer of an oil refinery license from a legal entity equipped with a Refinery Concession License to another legal entity shall be made only if the legal entity has fulfilled its legal and financial obligations towards state bodies and after approval by the ministry responsible for hydrocarbons, according to the conditions and procedures set out in this decision.

2. The transfer of the Refinery Concession License shall be made after the legal entity to which it is transferred meets the requirements set out in the documentation on the basis of which the concession license was initially granted, except in cases where these requirements refer to conditions that are no longer necessary to be met. In any case, the documentation submitted by the legal entity to which the license is transferred must guarantee that the technical parameters of the project will be implemented, the project implementation

deadline, environmental standards and other obligations provided for in the Refinery Concession License will be respected.

3. The Refinery Concession License Holder and the legal entity to which it will be transferred shall submit to the ministry responsible for hydrocarbons a joint request for transfer, accompanied by the documentation of the entity to which the concession license is requested to be transferred, proving the fulfillment of the requirements provided for in points 1.1, 1.2, 1.4, 1.6, 1.7, 1.9 and 1.10, of point 1, of chapter III, of this decision, as well as any other documentation proving the financial support for the entity to which the transfer is made. The supporting documents must be drawn up in Albanian, original or notarized photocopies. For documents translated into Albanian, the certification of the translator's signature is made by a notary.

The structure responsible for hydrocarbons in the ministry responsible for hydrocarbons verifies the documentation and the fulfillment of the conditions set out in points 2 and 3 of this chapter.

4. When the documents are complete and regular, the minister responsible for hydrocarbons approves the transfer of the relevant concession license according to the terms and procedures of this decision.

5. The deadline for verifying the documentation, as well as completing the procedural and administrative practice for the transfer of the relevant concession license cannot be more than 60 (sixty) days from the date of receipt of the joint request of two legal entities.

6. When the verification of data and indicators shows that the required conditions are not met, the submitted documents shall be returned to the entities, no later than 60 (sixty) days from the date of receipt of the request. Legal entities may resubmit the documents after completing them within a period not exceeding 90 (ninety) days from the date of notification of the completion of the documentation.

In the event that legal entities do not submit the required documentation within the specified period of 90 (ninety) days, the ministry responsible for hydrocarbons shall reject this request. Legal entities have the right to file an appeal with the competent court, within 30 (thirty) days from the date of rejection of the request.

7. The Refinery Concession License, after approval of the transfer, shall contain the data required for are specified in point 4, of Chapter III, of this decision, by changing the information related to the legal entity benefiting from the concession permit.

The Refinery Concession License, after the approval of the transfer, is a document with the same number, but with a fraction, of the previous concession license document that the legal entity has received. The Refinery Concession License is drawn up in three copies, of which one copy is kept in the ministry responsible for hydrocarbons and one copy is officially forwarded to the legal entity to which the concession license is granted and to the Council of Ministers.

V. PROCEDURES FOR RENEWAL OF THE REFINERY CONCESSION LICENSE

1. The legal entity equipped with the Refinery Concession License has the right to renew it, through the submission of a request by the legal entity, no later than 1 year before the expiration of the license.

2. The Refinery Concession License Holder shall submit to the Ministry responsible for hydrocarbons the request for renewal of the license, accompanied by the documentation specified in points 1.1, 1.2, 1.4, 1.6, 1.7, 1.9 and 1.10, of point 1, of Chapter III, of this decision. The entity shall also submit a certificate of compliance with the technical conditions and norms, in terms of the safe operation of the refinery, occupational safety and guaranteeing the quality of by-products, issued by the responsible body.

The supporting documents shall be drawn up in Albanian, originals or notarized photocopies. For documents translated into Albanian, the certification of the translator's signature shall be made by a notary.

3. The request for the renewal of the Refinery Concession License together with all documents is reviewed by the structure responsible for hydrocarbons in the ministry responsible for hydrocarbons.

4. The renewal of the Refinery Concession License is made against payment of 15,000,000 (fifteen million) lek by the legal entity, the amount of which is paid entirely to the state budget.

VI. FINAL PROVISIONS

1. Decision No. 553, dated 12.8.2004, of the Council of Ministers, "On the procedures and conditions for granting concession permits for the construction and use of refineries, oil pipelines and gas pipelines", as amended, is repealed.

2. The provisions of Decision No. 553, dated 12.8.2004, of the Council of Ministers, "On the procedures and conditions for granting concession permits for the construction and use of refineries, oil pipelines and gas pipelines", as amended, shall apply to the procedures for granting concession licenses for refineries, the applications for which have been filed with the ministry responsible for hydrocarbons before the entry into force of this decision.

3. The Ministry of Energy and Industry is hereby charged with the implementation of this decision.

This decision shall enter into force upon its publication in the Official Gazette.

PRIME MINISTER

Edi Rama

Porto Romano Refinery Project – Executive Summary

Project Name: Porto Romano Refinery

Location: Porto Romano, Durrës, Albania

Developer: Oil Palmir JSC

Official Representative: Edidani LLC

Owner and CEO: Shani Shehu

Direct Contact:

- Phone (WhatsApp / Direct): +1 (817) 538-7697
- Email: Italyfic@gmail.com

Project Overview:

The Porto Romano Refinery will be a **150,000 barrels per day (BPD)** state-of-the-art crude oil refinery, strategically located near Durrës, Albania's largest port city.

The facility will leverage Albania's growing energy sector, local oil fields, and strategic position on the Adriatic Sea to create a regional fuel and energy hub.

Key Highlights:

- **Capacity:** 150,000 BPD
 - **Technology:** EU-compliant, eco-friendly (Euro 5 fuels)
 - **Strategic Location:** Near Porto Romano Deep-Sea Port and Pan-European Corridor VIII
 - **Investment Required:** Approx. \$3.3 billion USD
 - **Payback Period:** 4–6 years
 - **Environmental Commitment:** Carbon capture, zero-pollution action plan, renewable energy integration
 - **Social Impact:** 10,000 construction jobs and 2,500 permanent jobs created • **Export Markets:** Italy, Greece, Croatia, North Macedonia, Kosovo, Montenegro
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Investor Benefits:

- Full management control over the project and finances
 - Real-time financial transparency
 - Priority access to Albania's expanding energy logistics network
 - Strong regional fuel demand and low competition in Albania
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Next Steps:

Serious investors are invited to enter into direct discussions through **Edidani LLC**. All inquiries, project details, financials, and site visits are managed personally by **Shani Shehu**.

Contact Information:

- Phone: +1 (817) 538-7697 • Email: Italyfic@gmail.com

For OIL PALMIR JSC:

Title: CEO&OWNER Name:
Perparim Gropa

Signature:

The image shows a handwritten signature in blue ink next to an official blue circular stamp. The stamp contains the text "OIL PALMIR sh.a" in the center, with "127401403P" below it. The outer ring of the stamp reads "MINISTRI E TREGTISE DHE SHUMICE E PAJISE TE NAFTE" at the top and "TIRRE ALBANIA" at the bottom.

